## CAE 464/517 HVAC Systems Design Spring 2023

## April 11, 2023 <br> Hydronic systems: system characteristics and project questions

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Dr. Mohammad Heidarinejad, Ph.D., P.E. Illinois Institute of Technology muh182@iit.edu

## ANNOUNCEMENTS

## Announcements

- Assignment 5 is posted (optional)
- A new measurement activity will be posted (optional)
- Anyone opposed to change the exam time?

RECAP

## Recap

- What are the supply piping layouts (zone level)


## Recap

- What are the supply piping layouts (central)


## Recap

- Another approach is the series circuit with distributed load pumps:



## Recap



DESIGN PROCEDURE

## Design Procedure



## Design Procedure

## FRICTION LOSS IN WATER FITTINGS

## Friction Loss in Water Fittings

- Friction loss in a water pipe fitting is equal to:

$$
H_{l f}=K\left(\frac{V^{2}}{2 g}\right)
$$

Table 3 K Factors: Threaded Steel Pipe Fittings

| Nominal Pipe Dia., in. | $90^{\circ}$ Standard Elbow | $90^{\circ}$ LongRadius Elbow | $\begin{gathered} \mathbf{4 5}^{\circ} \\ \text { Elbow } \end{gathered}$ | Return <br> Bend | TeeLine | TeeBranch | Globe <br> Valve | Gate <br> Valve | Angle <br> Valve | Swing <br> Check <br> Valve | Bell Mouth Inlet | Square Inlet | Projected Inlet |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 3/8 | 2.5 | - | 0.38 | 2.5 | 0.90 | 2.7 | 20 | 0.40 | - | 8.0 | 0.05 | 0.5 | 1.0 |
| 1/2 | 2.1 | - | 0.37 | 2.1 | 0.90 | 2.4 | 14 | 0.33 | - | 5.5 | 0.05 | 0.5 | 1.0 |
| 3/4 | 1.7 | 0.92 | 0.35 | 1.7 | 0.90 | 2.1 | 10 | 0.28 | 6.1 | 3.7 | 0.05 | 0.5 | 1.0 |
| 1 | 1.5 | 0.78 | 0.34 | 1.5 | 0.90 | 1.8 | 9 | 0.24 | 4.6 | 3.0 | 0.05 | 0.5 | 1.0 |
| $11 / 4$ | 1.3 | 0.65 | 0.33 | 1.3 | 0.90 | 1.7 | 8.5 | 0.22 | 3.6 | 2.7 | 0.05 | 0.5 | 1.0 |
| $11 / 2$ | 1.2 | 0.54 | 0.32 | 1.2 | 0.90 | 1.6 | 8 | 0.19 | 2.9 | 2.5 | 0.05 | 0.5 | 1.0 |
| 2 | 1.0 | 0.42 | 0.31 | 1.0 | 0.90 | 1.4 | 7 | 0.17 | 2.1 | 2.3 | 0.05 | 0.5 | 1.0 |
| $21 / 2$ | 0.85 | 0.35 | 0.30 | 0.85 | 0.90 | 1.3 | 6.5 | 0.16 | 1.6 | 2.2 | 0.05 | 0.5 | 1.0 |
| 3 | 0.80 | 0.31 | 0.29 | 0.80 | 0.90 | 1.2 | 6 | 0.14 | 1.3 | 2.1 | 0.05 | 0.5 | 1.0 |
| 4 | 0.70 | 0.24 | 0.28 | 0.70 | 0.90 | 1.1 | 5.7 | 0.12 | 1.0 | 2.0 | 0.05 | 0.5 | 1.0 |

Source: Engineering Data Book (Hydraulic Institute 1990).

Is there a difference between open or close valve?

## Friction Loss in Water Fittings

- Friction loss in a water pipe fitting is equal to:

Table $4 \quad K$ Factors: Flanged Welded Steel Pipe Fittings

| Nominal Pipe <br> Dia., in. | $\begin{gathered} 90^{\circ} \\ \text { Standard } \\ \text { Elbow } \end{gathered}$ | $\mathbf{9 0}^{\circ}$ LongRadius Elbow | $45^{\circ}$ LongRadius Elbow | Return Bend Standard | Return Bend LongRadius | Tee- <br> Line | TeeBranch | Globe <br> Valve | Gate <br> Valve | Angle <br> Valve | Swing <br> Check <br> Valve |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1 | 0.43 | 0.41 | 0.22 | 0.43 | 0.43 | 0.26 | 1.0 | 13 | - | 4.8 | 2.0 |
| $11 / 4$ | 0.41 | 0.37 | 0.22 | 0.41 | 0.38 | 0.25 | 0.95 | 12 | - | 3.7 | 2.0 |
| $11 / 2$ | 0.40 | 0.35 | 0.21 | 0.40 | 0.35 | 0.23 | 0.90 | 10 | - | 3.0 | 2.0 |
| 2 | 0.38 | 0.30 | 0.20 | 0.38 | 0.30 | 0.20 | 0.84 | 9 | 0.34 | 2.5 | 2.0 |
| $21 / 2$ | 0.35 | 0.28 | 0.19 | 0.35 | 0.27 | 0.18 | 0.79 | 8 | 0.27 | 2.3 | 2.0 |
| 3 | 0.34 | 0.25 | 0.18 | 0.34 | 0.25 | 0.17 | 0.76 | 7 | 0.22 | 2.2 | 2.0 |
| 4 | 0.31 | 0.22 | 0.18 | 0.31 | 0.22 | 0.15 | 0.70 | 6.5 | 0.16 | 2.1 | 2.0 |
| 6 | 0.29 | 0.18 | 0.17 | 0.29 | 0.18 | 0.12 | 0.62 | 6 | 0.10 | 2.1 | 2.0 |
| 8 | 0.27 | 0.16 | 0.17 | 0.27 | 0.15 | 0.10 | 0.58 | 5.7 | 0.08 | 2.1 | 2.0 |
| 10 | 0.25 | 0.14 | 0.16 | 0.25 | 0.14 | 0.09 | 0.53 | 5.7 | 0.06 | 2.1 | 2.0 |
| 12 | 0.24 | 0.13 | 0.16 | 0.24 | 0.13 | 0.08 | 0.50 | 5.7 | 0.05 | 2.1 | 2.0 |

[^0]
## Friction Loss in Water Fittings

- Friction loss in a water pipe fitting is equal to:

Table 6 Summary of $\boldsymbol{K}$ Values for Steel Ells, Reducers, and Expansions

|  | Past ${ }^{\text {a }}$ | ASHRAE Research ${ }^{\text {b,c }}$ |  |  |
| :---: | :---: | :---: | :---: | :---: |
|  |  | 4 fps | 8 fps | 12 fps |
| 2 in. S.R. ${ }^{\text {e }}$ ell $(R / D=1)$ thread | 0.60 to $1.0(1.0)^{\text {d }}$ | 0.60 | 0.68 | 0.736 |
| 4 in. S.R. ell $(R / D=1)$ weld | 0.30 to 0.34 | 0.37 | 0.34 | 0.33 |
| 1 in. L.R. ell $(R / D=1.5)$ weld | to 1.0 | - | - | - |
| 2 in. L.R. ell $(R / D=1.5)$ weld | 0.50 to 0.7 | - | - | - |
| 4 in. L.R. ell $(R / D=1.5)$ weld | 0.22 to $0.33(0.22)^{\text {d }}$ | 0.26 | 0.24 | 0.23 |
| 6 in. L.R. ell $(R / D=1.5)$ weld | 0.25 | 0.26 | 0.24 | 0.24 |
| 8 in. L.R. ell $(R / D=1.5)$ weld | 0.20 to 0.26 | 0.22 | 0.20 | 0.19 |
| 10 in. L.R. ell $(R / D=1.5)$ weld | 0.17 | 0.21 | 0.17 | 0.16 |
| 12 in . L.R. ell $(R / D=1.5)$ weld | 0.16 | 0.17 | 0.17 | 0.17 |
| 16 in. L.R. ell $(R / D=1.5)$ weld | 0.12 | 0.12 | 0.12 | 0.11 |
| 20 in. L.R. ell $(R / D=1.5)$ weld | 0.09 | 0.12 | 0.10 | 0.10 |
| 24 in. L.R. ell $(R / D=1.5)$ weld | 0.07 | 0.098 | 0.089 | 0.089 |
| Reducer (2 by 1.5 in .) thread | - | 0.53 | 0.28 | 0.20 |
| ( 4 by 3 in.) weld | 0.22 | 0.23 | 0.14 | 0.10 |
| ( 6 by 4 in .) weld |  | 0.62 | 0.54 | 0.53 |
| ( 8 by 6 in.) weld |  | 0.31 | 0.28 | 0.26 |
| (10 by 8 in.) weld |  | 0.16 | 0.14 | 0.14 |
| ( 12 by 10 in .) weld | - | 0.14 | 0.14 | 0.14 |
| (16 by 12 in .) weld | - | 0.17 | 0.16 | 0.17 |
| ( 20 by 16 in.) weld | - | 0.16 | 0.13 | 0.13 |
| ( 24 by 20 in .) weld | - | 0.053 | 0.053 | 0.055 |
| Expansion (1.5 by 2 in.) thread | - | 0.16 | 0.13 | 0.02 |
| ( 3 by 4 in.) weld | - | 0.11 | 0.11 | 0.11 |
| (4 by 6 in.) weld | - | 0.28 | 0.28 | 0.29 |
| ( 6 by 8 in.) weld | - | 0.15 | 0.12 | 0.11 |
| ( 8 by 10 in .) weld | - | 0.11 | 0.09 | 0.08 |
| (10 by 12 in .) weld | - | 0.11 | 0.11 | 0.11 |
| ( 12 by 16 in.) weld | - | 0.073 | 0.076 | 0.073 |
| (16 by 20 in .) weld | - | 0.024 | 0.021 | 0.022 |
| ( 20 by 24 in .) weld | - | 0.020 | 0.023 | 0.020 |

${ }^{\text {ap }}$ Published data by Crane Co. (1988), Freeman (1941), and Hydraulic Institute (1990).
${ }^{\text {b }}$ Rahmeyer (1999a, 2002a).
${ }^{\text {CDing et al. (2005) }}$
d ( ) Data published in 1993 ASHRAE Handbook-Fundamentals.
${ }^{\text {e }}$ S.R.-short radius or regular ell; L.R.-long-radius ell.

## Friction Loss in Water Fittings

- We also sometimes define equivalent length:

$$
\begin{aligned}
& \text { Head loss in a pipe }=f \frac{L}{D} \frac{V^{2}}{2 g} \quad K=f \frac{L}{D}
\end{aligned}
$$

Head loss in a fitting $=K \frac{V^{2}}{2 g}$

- $\frac{L}{D}$ is the equivalent length in pipe diameters of straight pipe that will cause the same pressure drop as the valve or fitting under the same flow conditions


## Friction Loss in Water Fittings

- ASHRAE Chapter 22 has some list of equivalent lengths:

Table 27 Equivalent Length in Feet of Pipe for $90^{\circ}$ Elbows

| Velocity, <br> fps | $\mathbf{1 / 2}$ | $\mathbf{3} / \mathbf{4}$ | $\mathbf{1}$ | $\mathbf{1 1 / 4}$ | $\mathbf{1 1 / 2}$ | $\mathbf{2}$ | $\mathbf{2 ~ 1 / 2}$ | $\mathbf{3}$ | $\mathbf{3 1 / 2}$ | $\mathbf{4}$ | $\mathbf{5}$ | $\mathbf{6}$ | $\mathbf{8}$ | $\mathbf{1 0}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 1.2 | 1.7 | 2.2 | 3.0 | 3.5 | 4.5 | 5.4 | 6.7 | 7.7 | 8.6 | 10.5 | 12.2 | 15.4 | 18.7 |
| 2 | 1.4 | 1.9 | 2.5 | 3.3 | 3.9 | 5.1 | 6.0 | 7.5 | 8.6 | 9.5 | 11.7 | 13.7 | 17.3 | 20.8 |
| 3 | 1.5 | 2.0 | 2.7 | 3.6 | 4.2 | 5.4 | 6.4 | 8.0 | 9.2 | 10.2 | 12.5 | 14.6 | 18.4 | 22.3 |
| 4 | 1.5 | 2.1 | 2.8 | 3.7 | 4.4 | 5.6 | 6.7 | 8.3 | 9.6 | 10.6 | 13.1 | 15.2 | 19.2 | 23.2 |
| 5 | 1.6 | 2.2 | 2.9 | 3.9 | 4.5 | 5.9 | 7.0 | 8.7 | 10.0 | 11.1 | 13.6 | 15.8 | 19.8 | 24.2 |
| 6 | 1.7 | 2.3 | 3.0 | 4.0 | 4.7 | 6.0 | 7.2 | 8.9 | 10.3 | 11.4 | 14.0 | 16.3 | 20.5 | 24.9 |
| 7 | 1.7 | 2.3 | 3.0 | 4.1 | 4.8 | 6.2 | 7.4 | 9.1 | 10.5 | 11.7 | 14.3 | 16.7 | 21.0 | 25.5 |
| 8 | 1.7 | 2.4 | 3.1 | 4.2 | 4.9 | 6.3 | 7.5 | 9.3 | 10.8 | 11.9 | 14.6 | 17.1 | 21.5 | 20.3 |
| 9 | 1.8 | 2.4 | 3.2 | 4.3 | 5.0 | 6.4 | 7.7 | 9.5 | 11.0 | 12.2 | 14.9 | 17.4 | 21.9 | 26.6 |
| 10 | 1.8 | 2.5 | 3.2 | 4.3 | 5.1 | 6.5 | 7.8 | 9.7 | 11.2 | 12.4 | 15.2 | 17.7 | 22.2 | 27.0 |

## Friction Loss in Water Fittings

- ASHRAE Chapter 22 has some list of equivalent lengths:

Table 28 Iron and Copper Elbow Equivalents*

| Fitting | Iron Pipe | Copper Tubing |
| :--- | :---: | :---: |
| Elbow, $90^{\circ}$ | 1.0 | 1.0 |
| $45^{\circ}$ | 0.7 | 0.7 |
| $90^{\circ}$ long-radius | 0.5 | 0.5 |
| $90^{\circ}$ welded | 0.5 | 0.5 |
| Reduced coupling | 0.4 | 0.4 |
| Open return bend | 1.0 | 1.0 |
| Angle radiator valve | 2.0 | 3.0 |
| Radiator or convector | 3.0 | 4.0 |
| Boiler or heater | 3.0 | 4.0 |
| Open gate valve | 0.5 | 0.7 |
| Open globe valve | 12.0 | 17.0 |

Sources: Giesecke (1926) and Giesecke and Badgett (1931, 1932a).
*See Table 10 for equivalent length of one elbow.

## Equivalent Length

- ASHRAE Chapter 22 has some list of equivalent lengths:

Table 8 Test Summary for Loss Coefficients $K$ and
Equivalent Loss Lengths

| Schedule 80 PVC Fitting | $K$ | $L$, ft |
| :---: | :---: | :---: |
| Injected molded elbow, 2 in. | 0.91 to 1.00 | 8.4 to 9.2 |
| 4 in. | 0.86 to 0.91 | 18.3 to 19.3 |
| 6 in. | 0.76 to 0.91 | 26.2 to 31.3 |
| 8 in. | 0.68 to 0.87 | 32.9 to 42.1 |
| 8 in. fabricated elbow, Type I, components | 0.40 to 0.42 | 19.4 to 20.3 |
| Type II, mitered | 0.073 to 0.76 | 35.3 to 36.8 |
| 6 by 4 in. injected molded reducer | 0.12 to 0.59 | 4.1 to 20.3 |
| Bushing type | 0.49 to 0.59 | 16.9 to 20.3 |
| 8 by 6 in. injected molded reducer | 0.13 to 0.63 | 6.3 to 30.5 |
| Bushing type | 0.48 to 0.68 | 23.2 to 32.9 |
| Gradual reducer type | 0.21 | 10.2 |
| 4 by 6 in. injected molded expansion | 0.069 to 1.19 | 1.5 to 25.3 |
| Bushing type | 0.069 to 1.14 | 1.5 to 24.2 |
| 6 by 8 in. injected molded expansion | 0.95 to 0.96 | 32.7 to 33.0 |
| Bushing type | 0.94 to 0.95 | 32.4 to 32.7 |
| Gradual reducer type | 0.99 | 34.1 |

## CLASS ACTIVITY

## Class Activity

- Example: Size the pipe for the water distribution system shown below. The pipe is type L copper. Notice that the lengths given are the total equivalent lengths excluding the coil and control valves.

| Coil | Flow rate, <br> gpm (L/s) | Lost head, ft (m) |  |
| :---: | :---: | :---: | :---: |
|  |  | Coil | Control <br> valve |
| A | $40(2.5)$ | $12(3.7)$ | $10(3)$ |
| B | $40(2.5)$ | $15(4.6)$ | $12(3.7)$ |
| C | $50(3.2)$ | $18(5.5)$ | $15(4.6)$ |



## Class Activity

- Solution:
$\square$ Consider all the routes



## Class Activity

- Solution:

Calculate the flow rate in each section:

Pipe Section No.
Flow rate(gpm)
1-2
2-3
3-4
4-5
Common pipe
2-6
3-7
7-8

## Class Activity

- Solution:

Calculate the flow rate in each section:

Pipe Section No.
1-2

$$
Q_{\text {total }}=Q_{A}+Q_{B}+Q_{C}=40+40+50=130
$$

2-3

$$
Q_{\text {total }}-Q_{A}=130-40=90
$$

3-4
4-5

$$
\begin{gathered}
Q_{C}=50 \\
Q_{\text {total }}=130
\end{gathered}
$$

Common pipe

## 0

2-6
$Q_{A}=40$
3-7
$Q_{B}=40$
7-8

$$
Q_{A}+Q_{B}=80
$$

## Class Activity

- Solution:

Identify the pipe diameter and head loss ft/100-ft of each section (Figure 15 - Chapter 22):

| Pipe section <br> No. | Flow rate <br> $(\mathbf{g p m})$ | Nominal size <br> (in) | Lost head per 100 ft <br> $(\boldsymbol{f t} / \mathbf{1 0 0 f t})$ |
| :---: | :---: | :---: | :---: |
| $\mathbf{1 - 2}$ | 130 |  |  |
| $\mathbf{2 - 3}$ | 90 |  |  |
| $\mathbf{3 - 4}$ | 50 |  |  |
| $\mathbf{4 - 5}$ | 130 |  |  |
| Common pipe | 0 |  |  |
| $\mathbf{2 - 6}$ | 40 |  |  |
| $\mathbf{3 - 7}$ | 40 |  |  |
| $\mathbf{7 - 8}$ | 80 |  |  |

## Class Activity

- Solution:
$\square$ Identify the pipe diameter and head loss $\mathrm{ft} / 100-\mathrm{ft}$ of each section (Figure 15 - Chapter 22):


Fig. 15 Friction Loss for Water in Copper Tubing (Types K, L, M)

## Class Activity

- Solution:
$\square$ Identify the pipe diameter and head loss ft/100-ft of each section (Figure 15 - Chapter 22):

| Pipe section <br> No. | Flow rate <br> (gpm) | Nominal size <br> (in) | Lost head per 100 ft <br> $(\boldsymbol{f t} / \mathbf{1 0 0} \boldsymbol{f t})$ |
| :---: | :---: | :---: | :---: |
| $\mathbf{1 - 2}$ | 130 | 3 | 3.7 |
| $\mathbf{2 - 3}$ | 90 | $21 / 2$ | 4.8 |
| $\mathbf{3 - 4}$ | 50 | 2 | 5.0 |
| $\mathbf{4 - 5}$ | 130 | 3 | 3.7 |
| Common pipe | 0 | 3 | $\ldots .$. |
| $\mathbf{2 - 6}$ | 40 | 2 | 3.4 |
| $\mathbf{3 - 7}$ | 40 | 2 | 3.4 |
| $\mathbf{7 - 8}$ | 80 | $21 / 2$ | 3.9 |

## Class Activity

- Solution:

Calculate the head loss for each path:

| Pipe section No. | Flow rate (gpm) | Nominal size (in) | $\begin{aligned} & \text { Lost head per } \\ & 100 \mathrm{ft}(\mathrm{ft} / \\ & 100 \mathrm{ft}) \end{aligned}$ | Pipe equivalent length ( $L_{e}(\mathrm{ft})$ ) | Lost head of pipe, coil and control valve (ft) | Total loss head (ft) |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1-2 | 130 | 3 | 3.7 | 60 | $60 \times 3.7 / 100=2.2$ | 39.2 |
| 2-3 | 90 | $21 / 2$ | 4.8 | 20 | $20 \times 4.8 / 100=1.0$ |  |
| 3-4 | 50 | 2 | 5.0 | 30 | $30 \times 5.0 / 100=1.5$ |  |
| Coil C | $\ldots$ | $\ldots$ | $\ldots$ | $\ldots$ | 18 |  |
| Con. C | $\ldots$ | $\ldots$ | $\ldots$ | .... | 15 |  |
| 4-5 | 130 | 3 | 3.7 | 40 | $40 \times 3.7 / 100=1.5$ |  |
| Common pipe | 0 | 3 | $\ldots$ | $\ldots$ | 0 |  |
| 2-6 | 40 | 2 | 3.4 | 30 | $30 \times 3.4 / 100=1.0$ | 23 |
| Coil A | $\ldots$ | $\ldots$ | $\ldots$ | $\ldots$ | 12 |  |
| Con. A | $\ldots$. | . | $\ldots$ | . | 10 |  |
| 3-7 | 40 | 2 | 3.4 | 10 | $10 \times 3.4 / 100=0.5$ | 28.3 |
| Coil B | .... | .... | .... | .... | 15 |  |
| Con. B | $\ldots$ | $\ldots$ | $\ldots$ | $\ldots$ | 12 |  |
| 7-8 | 80 | $21 / 2$ | 3.9 | 20 | $20 \times 3.9 / 100=0.8$ |  |

## MORE ON FITTINGS

## More on Fittings

- Unfortunately, ASHRAE Chapter 22 does not have all the fittings. We can rely on different resources. For example:
$\square$ Source 1: Engineering Toolbox
$\square$ Source 2: McQuiston et al. Heating Ventilating and Air Conditioning, $5^{\text {th }}$ Edition
Source 3: Reddy et al., Heating and Cooling of Buildings, 3rd Edition


## More on Fittings

- Source 1: Engineering Toolbox

| Equivalent Length of Straight Pipe for Valves and Fittings (feet) |  |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Screwed Fittings |  | Pipe Size |  |  |  |  |  |  |  |  |  |  |
|  |  | 1/4 | 3/8 | 1/2 | 3/4 | 1 | $11 / 4$ | $11 / 2$ | 2 | $21 / 2$ | 3 | 4 |
| Elbows | Regular 90 deg | 2.3 | 3.1 | 3.6 | 4.4 | 5.2 | 6.6 | 7.4 | 8.5 | 9.3 | 11.0 | 13.0 |
|  | Long radius 90 deg | 1.5 | 2.0 | 2.2 | 2.3 | 2.7 | 3.2 | 3.4 | 3.6 | 3.6 | 4.0 | 4.6 |
|  | Regular 45 deg | 0.3 | 0.5 | 0.7 | 0.9 | 1.3 | 1.7 | 2.1 | 2.7 | 3.2 | 4.0 | 5.5 |
| Tees | Line flow | 0.8 | 1.2 | 1.7 | 2.4 | 3.2 | 4.6 | 5.6 | 7.7 | 9.3 | 12.0 | 17.0 |
|  | Branch flow | 2.4 | 3.5 | 4.2 | 5.3 | 6.6 | 8.7 | 9.9 | 12.0 | 13.0 | 17.0 | 21.0 |
| Retum Bends | Regular 180 deg | 2.3 | 3.1 | 3.6 | 4.4 | 5.2 | 6.6 | 7.4 | 8.5 | 9.3 | 11.0 | 13.0 |
| Valves | Globe | 21.0 | 22.0 | 22.0 | 24.0 | 29.0 | 37.0 | 42.0 | 54.0 | 62.0 | 79.0 | 110.0 |
|  | Gate | 0.3 | 0.5 | 0.6 | 0.7 | 0.8 | 1.1 | 1.2 | 1.5 | 1.7 | 1.9 | 2.5 |
|  | Angle | 12.8 | 15.0 | 15.0 | 15.0 | 17.0 | 18.0 | 18.0 | 18.0 | 18.0 | 18.0 | 18.0 |
|  | Swing Check | 7.2 | 7.3 | 8.0 | 8.8 | 11.0 | 13.0 | 15.0 | 19.0 | 22.0 | 27.0 | 38.0 |
| Strainer |  |  | 4.6 | 5.0 | 6.6 | 7.7 | 18.0 | 20.0 | 27.0 | 29.0 | 34.0 | 42.0 |

engineeringtoolbox.com

## More on Fittings

- Source 1: Engineering Toolbox

| Equivalent Length of Straight Pipe for Valves and Fittings (feet) |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Flanged Fittings |  | Pipe Size |  |  |  |  |  |  |  |  |  |  |  |  |
|  |  | 1/2 | 3/4 | 1 | $11 / 4$ | $11 / 2$ | 2 | $21 / 2$ | 3 | 4 | 5 | 6 | 8 | 10 |
| Elbows | Regular 90 deg | 0.9 | 1.2 | 1.6 | 2.1 | 2.4 | 3.1 | 3.6 | 4.4 | 5.9 | 7.3 | 8.9 | 12 | 14 |
|  | Long radius 90 deg | 1.1 | 1.3 | 1.6 | 2.0 | 2.3 | 2.7 | 2.9 | 3.4 | 4.2 | 5 | 5.7 | 7 | 8 |
|  | Regular 45 deg | 0.5 | 0.6 | 0.8 | 1.1 | 1.3 | 1.7 | 2.0 | 2.6 | 3.5 | 4.5 | 5.6 | 7.7 | 9 |
| Tees | Line flow | 0.7 | 0.8 | 1.0 | 1.3 | 1.5 | 1.8 | 1.9 | 2.2 | 2.8 | 3.3 | 3.8 | 4.7 | 5.2 |
|  | Branch flow | 2.0 | 2.6 | 3.3 | 4.4 | 5.2 | 6.6 | 7.5 | 9.4 | 12.0 | 15 | 18 | 24 | 30 |
| Retum Bends | Regular 180 deg | 0.9 | 1.2 | 1.6 | 2.1 | 2.4 | 3.1 | 3.6 | 4.4 | 5.9 | 7.3 | 8.9 | 12 | 14 |
|  | Long radius 180 deg | 1.1 | 1.3 | 1.6 | 2.0 | 2.3 | 2.7 | 2.9 | 3.4 | 4.2 | 5 | 5.7 | 7 | 8 |
| Valves | Globe | 38.0 | 40.0 | 45.0 | 54.0 | 59.0 | 70.0 | 77.0 | 94.0 | 120.0 | 150 | 190 | 260 | 310 |
|  | Gate |  |  |  |  |  | 2.6 | 2.7 | 2.8 | 2.9 | 3.1 | 3.2 | 3.2 | 3.2 |
|  | Angle | 15.0 | 15.0 | 17.0 | 18.0 | 18.0 | 21.0 | 22.0 | 28.0 | 38.0 | 50 | 63 | 90 | 120 |

engineeringtoolboxcom

## More on Fittings

- Source 2: McQuiston et al. Heating Ventilating and Air Conditioning, 5th Edition

Globe and angle valves

Gate valves
wedge disc, double disc or plug type


If: $\beta-1, \theta=0, K_{1}=8 f t$
$\beta<1$ and $\theta<45^{\circ}, K_{2}=$ Formula 1
$\beta<1$ and $\theta>45^{\circ}<180^{\circ}, K_{2}=$ Formula 2


If: $\beta-1, K_{1}=340 \times f_{t}$


$$
\text { If: } \begin{aligned}
& \beta=1, \theta=0, K_{1}=3 \times f_{t} \\
& \beta<1 \text { and } \theta<45^{\circ}, K_{2}=\text { Formula 1 } \\
& \beta<1 \text { and } \theta>45^{\circ}<180^{\circ}, K_{2}=\text { Formula } 2
\end{aligned}
$$

## More on Fittings

- Source 2: McQuiston et al. Heating Ventilating and Air Conditioning, 5th Edition
Pipe enxit

Sharp-edged

Rounded

$$
K=1.0
$$

$$
K=1.0
$$

$$
K=1.0
$$

Standard elbows

$K=30 f t$

$K=16 \mathrm{ft}$

$90^{\circ}$ Pipe bends and flanged or butt-welding $90^{\circ}$ elbows


The resistance coefficient $K_{B}$ for pipe bends other than $90^{\circ}$ may be determined as follows:

$$
K_{B}=(n-1)\left(0.25 \pi f_{T} \frac{r}{D}+0.5 K\right)+K
$$

$n=$ number of $90^{\circ}$ bends
$K=$ resistance coefficient for one $90^{\circ}$ bend (per table)

## More on Fittings

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## More on Fittings

- Source 2: McQuiston et al. Heating Ventilating and Air Conditioning, 5th Edition

Table 10-2 Formulas, Definition of Terms, and Values of ft for
Fig. 10-22

$$
\begin{aligned}
& \text { Formula 1: } K_{2}=\frac{K_{1}+\left(\sin \frac{\theta}{2}\right) 0.8\left(1-\beta^{2}\right)+2.6\left(1-\beta^{2}\right)^{2}}{\beta^{4}} \\
& \text { Formula 2: } K_{2}=\frac{K_{1}+0.5\left(\sin \frac{\theta}{2}\right)\left(1-\beta^{2}\right)+\left(1-\beta^{2}\right)^{2}}{\beta^{4}} \\
& \beta=\frac{D_{1}}{D_{2}} ; \quad \beta^{2}=\left(\frac{D_{1}}{D_{2}}\right)^{2}=\frac{A_{1}}{A_{2}} ; \quad \begin{array}{l}
D_{1}=\text { smaller diameter } \\
A_{1}=\text { smaller area }
\end{array}
\end{aligned}
$$

| Nominal <br> Size, in. | Friction <br> Factor $f_{t}$ | Nominal <br> Size, in. | Friction <br> Factor $f_{t}$ |
| :---: | :---: | :---: | :---: |
| $\frac{1}{2}$ | 0.027 | 4 | 0.017 |
| $\frac{3}{4}$ | 0.025 | 5 | 0.016 |
| 1 | 0.023 | 6 | 0.015 |
| $1 \frac{1}{4}$ | 0.022 | $8-10$ | 0.014 |
| $1 \frac{1}{2}$ | 0.021 | $12-16$ | 0.013 |
| 2 | 0.019 | $18-24$ | 0.012 |
| $2 \frac{1}{2}, 3$ | 0.018 |  |  |

## More on Fittings

- Source 3: Reddy et al. Heating and Cooling of Buildings, 3rd Edition

|  | Nominal Pipe Size (in) |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 1/2 | $3 / 4$ | 1 | $11 / 4$ | $11 / 2$ | 2 | $21 / 2$ | 3 | 4 | 5 | 6 |
| 45 elbow | 0.8 | 0.9 | 1.3 | 1.7 | 2.2 | 2.8 | 3.3 | 4.0 | 5.5 | 6.6 | 8.0 |
| 90 elbow (Standard) | 1.6 | 2.0 | 2.6 | 3.3 | 4.3 | 5.5 | 6.5 | 8.0 | 11.0 | 13.0 | 16.0 |
| 90 elbow (long) | 1.0 | 1.4 | 1.7 | 2.3 | 2.7 | 3.5 | 4.2 | 5.2 | 7.0 | 8.4 | 10.4 |
| Gate valve open | 0.7 | 0.9 | 1.0 | 1.5 | 1.8 | 2.3 | 2.8 | 3.2 | 4.5 | 6.0 | 7.0 |
| Globe valve open | 17 | 22 | 27 | 36 | 43 | 55 | 67 | 82 | 110 | 134 | 164 |
| Angle valve | 7 | 9 | 12 | 15 | 18 | 24 | - | - | - | - | - |
| Tee-side flow | 3 | 4 | 5 | 7 | 9 | 12 | 14 | 17 | 22 | 28 | 34 |
| Swing check valve | 6 | 8 | 10 | 14 | 16 | 20 | 25 | 30 | 40 | 50 | 60 |
| Tee-straight throughflow | 1.6 | 2.0 | 2.6 | 3.3 | 4.3 | 5.5 | 6.5 | 8.0 | 11.0 | 13.0 | 16.0 |
| Radiator angle valve | 3 | 6 | 8 | 10 | 13 | - | - | - | - | - | - |
| Diverting tee | - | 20 | 14 | 11 | 12 | 14 | 14 | 14 | - | - | - |
| Flow check valve | - | 27 | 42 | 60 | 63 | 83 | 104 | 125 | 126 |  |  |

## PRIMARY - SECONDARY PUMPING

## Primary Secondary Pumping

- Was developed by Bell \& Gossett in 1954 as a method to increase system temperature drops, decrease total pump power requirements and increase system controllability
- Systems utilizing low or medium temperatures were allowed due to Primary - Secondary pumping
- Most modern systems utilize some variation of Primary Secondary pumps


## Primary Secondary Pumping

- Common Piping:
- Interconnects the primary to the secondary circuit
- Should have minimal to no pressure drop
- Hydraulically disconnects the two piping loops
- Flow in one loop will not cause flow in the other loop



## Primary Secondary Pumping

- Secondary pipe pump sized for pressure drops A-B, BC, C-D, D-E, E-G, G-H, H-I
- I-A should have no pressure drop



## Primary Secondary Pumping

- In hydronic systems, we use this strategy:



## Primary Secondary Pumping

- In hydronic systems, we use this strategy:

Primary flow equal to secondary flow


PUMPS

## Intro to Pumps

- Pumps provide differential pressure by converting electrical energy to move water



## Intro to Pumps

- Positive displacement pumps
$\square$ Rotary-type pumps
$\square$ Reciprocating-type pump

- Rotodynamic pumps
- Centrifugal pump
- Radial flow pump
- Axial flow pump
- Mixed flow pump


Figure 2. Volute case design

## Centrifugal Pumps



## Centrifugal Pumps

- Most common use in HVAC industry
- Chilled water
- Cooling tower


Figure 2. Volute case design

- Basic Principle
$\square$ Water enters impeller at low velocity \& pressure
$\square$ Water thrown outward by centrifugal force
$\square$ Water leaves at high velocity \& pressure


## Centrifugal Pumps

- Impeller types


Figure 1. Impeller Types (I to r): Open, Semi-Enclosed (or Semi-Open), Enclosed.

## Centrifugal Pumps

- It needs to be base mounted:



## SYSTEM CURVE

## System Curve

- Assume there is only friction and no change in elevation (no static lift)

- How is the system curve?



## System Curve

- How is the system curve for this one?



## System Curve

- System curve can change over time



## System Curve

- System curve can change over time


Figure 4
Flow (GPM)

PROJECT

Project


[^0]:    Source: Engineering Data Book (Hydraulic Institute 1990).

