## CAE 208 / MMAE 320: Thermodynamics Fall 2023

## November 16, 2023 <br> Entropy (2)

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## ANNOUNCEMENTS

## Announcements

- The extended deadline for Assignment 8 is tonight
- Assignment 9 is posted (2-3 days more extension is fine to submit it on Friday after the Thanksgiving)
- The bonus activities document is posted. Please pay attention to the deadlines and also the updates about this task

RECAP

## Recap

- The Reversed Carnot Cycle

The Carnot heat-engine cycle is a totally reversible cycle
Therefore, all the processes that comprise it can be reversed, in which case it becomes the Carnot refrigeration cycle

$P$-V diagram of the Carnot cycle

$P-V$ diagram of the reversed Carnot cycle

## Recap

- Any heat engine:

$$
\eta_{t h}=\frac{W}{Q_{H}}=1-\frac{Q_{L}}{Q_{H}}
$$

- Any Carnot heat engine:

$$
\eta_{t h, r e v}=1-\frac{T_{L}}{T_{H}}
$$

## Recap

- We can say:

$$
\eta_{t h}= \begin{cases}<\eta_{\text {th,rev }} & \text { irreversible heat engine } \\ =\eta_{\text {th,rev }} & \text { reversible heat engine } \\ >\eta_{\text {th,rev }} & \text { impossible heat engine }\end{cases}
$$

QUIZZ

## ENTROPY

## Entropy

- Objectives of Chapter 8:
- Apply the second law of thermodynamics to processes

Define a new property called entropy to quantify the secondlaw effects
Establish the increase of entropy principle
$\square$ Calculate the entropy changes that take place during processes for pure substances, incompressible substances, and ideal gases

- Examine a special class of idealized processes, called isentropic processes, and develop the property relations for these processes
Derive the reversible steady-flow work relations
$\square$ Develop the isentropic efficiencies for various steady-flow devices
Introduce and apply the entropy balance to various systems


## Entropy

- While the first law of thermodynamics deals with the property "energy" and "the conservation of it", the second law leads to the definition of a new property called "entropy"
- Entropy is somewhat an abstract property, and it is difficult to give a physical description of it without considering the microscopic state of the system
- Entropy is best understood and appreciated by studying its uses in commonly encountered engineering processes, and this is what we intend to do


## Entropy

- The equality in the Clausius inequality holds for totally or just internally reversible cycles and the inequality for the irreversible ones


$$
\oint \frac{\delta Q}{T} \leq 0
$$

## Entropy

- The equality in the Clausius inequality holds for totally or jut internally reversible cycles and the inequality for the irreversible ones

$$
\left(\oint \frac{\delta Q}{T}\right)_{\text {int }, \text { rev }}=0
$$

## Entropy

- Let's try to find out more about entropy with looking at work in a cycle:

$$
\begin{aligned}
& \oint d V=? \\
& \oint d V=\Delta V_{c y c l e}=0
\end{aligned}
$$

How about $\delta W$ ?

## Entropy

- Let's try to find out more about entropy with looking into a cycle:

$$
\begin{gathered}
d S=\oint \frac{\delta Q}{T} \quad\left(\frac{k J}{K}\right) \\
\Delta S=S_{2}-S_{1}=\int_{1}^{2}\left(\frac{\delta Q}{T}\right)_{i n t, r e v}
\end{gathered}
$$

## Entropy

- Pay attention to reversible and irreversible integration:



## Entropy

- A special case: Internally reversible isothermal heat transfer processes:

$$
\begin{gathered}
\Delta S=\int_{1}^{2}\left(\frac{\delta Q}{T}\right)_{\text {int }, r e v}=\int_{1}^{2}\left(\frac{\delta Q}{T_{0}}\right)_{\text {int }, r e v}=\frac{1}{T_{0}} \int_{1}^{2} \delta Q_{i n t, r e v} \\
\Delta S_{\text {isothermal }}=\frac{Q}{T_{0}} \quad\left(\frac{k J}{K}\right)
\end{gathered}
$$

(A reservoir can absorb or supply heat indefinitely at a constant temperature)

## Entropy

- For example, a piston-cylinder device contains a liquidvapor mixture of water at 300 K . During a constant pressure process, 750 kJ of heat is transferred to the water. As a result of the liquid in the cylinder vaporizes. Determine the entropy change of water during this process.


$$
\begin{gathered}
\Delta S_{\text {isothermal }}=\frac{Q}{T_{0}} \quad\left(\frac{\mathrm{~kJ}}{\mathrm{~K}}\right) \\
\Delta S=\frac{750 \mathrm{~kJ}}{300 \mathrm{~K}}=2.5 \frac{\mathrm{~kJ}}{\mathrm{~K}}
\end{gathered}
$$

## ENTROPY CHANGE OF PURE SUBSTANCES

## Entropy Change of Pure Substances

- Entropy is a property:



## Entropy Change of Pure Substances

- Entropy is a property:



## Entropy Change of Pure Substances

- For a closed system ( $m=$ constant $)$, during a process we have:

$$
\Delta S=m \Delta s=m\left(s_{2}-s_{1}\right)
$$

## THE INCREASE OF ENTROPY PRINCIPLE

## The Increase of Entropy Principle

- For processes we can write:

$$
\begin{aligned}
& \oint \frac{\delta Q}{T} \leq 0 \\
& \oint_{1}^{2} \frac{\delta Q}{T}+\left(\oint_{2}^{1} \frac{\delta Q}{T}\right)_{\text {int,rev }} \leq 0 \\
& \oint_{1}^{2} \frac{\delta Q}{T} \leq S_{2}-S_{1}
\end{aligned}
$$



$$
\oint_{1}^{2} \frac{\delta Q}{T} \leq d S
$$

## The Increase of Entropy Principle

- For entropy, we can say

$$
\begin{aligned}
& \oint_{1}^{2} \frac{\delta Q}{T} \leq \Delta S \\
& \Delta S_{s y s}=S_{2}-S_{1}=\oint_{1}^{2} \frac{\delta Q}{T}+S_{g e n}
\end{aligned}
$$

## The Increase of Entropy Principle

- Increase of entropy principle:

$$
\Delta S_{\text {isolated }} \geq 0
$$

## The Increase of Entropy Principle

- Entropy is an extensive property (not entropy per unit mass), so the total entropy of a system is equal to the sum of the entropies of the parts of the system (i.e., an isolated system may consist of any number of subsystem
(Isolated)



## The Increase of Entropy Principle

- For an isolated system:

$$
S_{\text {gen }}=\Delta S_{\text {total }}=\Delta S_{\text {sys }}+\Delta S_{\text {surr }} \geq 0
$$



## The Increase of Entropy Principle

- For an isolated system:



## The Increase of Entropy Principle

- The increase of entropy principle can be summarized as:

$$
S_{\text {gen }}=\left\{\begin{array}{l}
>0 . \\
=0 \quad \text { irreversible process } \\
<0 . \\
\text { reversible process } \\
<0 \text { impossible process }
\end{array}\right.
$$

## CLASS ACTIVITY

## Class Activity

- A rigid tank contains $5-\mathrm{kg}$ of refrigerant $134-\mathrm{a}$ at $20^{\circ} \mathrm{C}$ and 140 kPa . The refrigerant is now cooled while being stirred until its pressure drops to 100 kPa . Determine the entropy change of the refrigerant during this process.


## Class Activity

- Solutions (assumptions):
- Closed system ( $\mathrm{m}=$ constant)




## Class Activity

- Solutions (Calculations):

$$
\begin{aligned}
& \left\{\begin{array}{lll} 
& \\
P_{1}=140 \mathrm{kPa} \\
T_{1}=20^{\circ} \mathrm{C}
\end{array} \rightarrow \begin{array}{l}
s_{1}=1.0625 \frac{\mathrm{~kJ}}{\mathrm{~kg}-\mathrm{K}} \\
\end{array} \quad v_{1}=0.16544 \frac{\mathrm{~m}^{3}}{\mathrm{~kg}} .\right. \\
& \left\{\begin{array}{c} 
\\
P_{2}=100 \mathrm{kPa} \\
v_{2}=v_{1}
\end{array} \rightarrow \begin{array}{l}
v_{f}=0.0007258 \frac{\mathrm{~m}^{3}}{\mathrm{~kg}} \\
\\
v_{g}=0.19255 \frac{\mathrm{~m}^{3}}{\mathrm{~kg}}
\end{array}\right. \\
& \left(v_{f}<v_{2}<v_{g}\right)
\end{aligned}
$$

## Class Activity

- Solutions (Calculations):

$$
\begin{aligned}
& x_{2}=\frac{v_{2}-v_{f}}{v_{f g}}=\frac{0.16544-0.0007258}{0.19255-0.0007258}=0.859 \\
& s_{2}=s_{f}+x_{2} s_{f g}=(0.07182)+(0.859)(0.88008)=0.8278 \frac{\mathrm{~kJ}}{\mathrm{~kg}-\mathrm{K}}
\end{aligned}
$$

$$
\Delta S=m\left(s_{2}-s_{1}\right)=(5 \mathrm{~kg})\left(0.8278-1.0625 \frac{k J}{\mathrm{~kg}-K}\right)=-1.173 \mathrm{~kJ} / \mathrm{K}
$$

## CLASS ACTIVITY

## Class Activity

- A piston-cylinder device initially contains 3 lbm of liquid water at 20 psia and $70^{\circ} \mathrm{F}$. The water is now heated at constant pressure by the addition of 3450 Btu of heat. Determine the entropy change of the water during this process.


## Class Activity

- Solutions (assumptions):
$\square$ The tank is stationary and thus the kinetic and potential energy changes are zero $(\triangle K E=\Delta P E=0)$
$\square$ The process is quasi-equilibrium
$\square$ The pressure remains constant during this process $\left(P_{1}=P_{2}\right)$



## Class Activity

- Solutions (processes):



## Class Activity

- Solutions (Calculation):

$$
\begin{aligned}
& P_{1}=20 \text { psia } \\
& T_{1}=70^{\circ} \mathrm{F}
\end{aligned} \rightarrow \quad s_{1} \cong s_{f @ 70^{\circ} \mathrm{F}}=0.07459 \frac{\mathrm{Btu}}{\mathrm{lbm}-R}
$$

## Class Activity

- Solutions (Calculation):

$$
\begin{aligned}
& E_{\text {in }}-E_{\text {out }}=\Delta E_{\text {system }} \\
& Q_{\text {in }}-W_{b}=\Delta \mathrm{U} \\
& Q_{\text {in }}=\Delta \mathrm{H}=\mathrm{m}\left(\mathrm{~h}_{2}-\mathrm{h}_{1}\right) \\
& 3450 \mathrm{Btu}=(3 \mathrm{lbm})\left(h_{2}-38.08 \frac{\mathrm{Btu}}{\mathrm{lbm}}\right) \\
& h_{2}=1188.1 \frac{\mathrm{Btu}}{\mathrm{lbm}}
\end{aligned}
$$

## Class Activity

- Solutions (Calculation):

$$
\begin{aligned}
& P_{1}=20 \text { psia } \\
& h_{2}=1188.1 \frac{\mathrm{Btu}}{\mathrm{lbm}} \quad \rightarrow \quad \quad s_{2}=1.7761 \frac{\text { Btu }}{\text { lbm }-R} \\
& \text { (From Table } A-6 A-\text { interpolation) }
\end{aligned}
$$

$$
\Delta S=m\left(s_{2}-s_{1}\right)=(3 \mathrm{lbm})\left(1.7761-0.07459 \frac{B t u}{l b m-R}\right)=5.105 \frac{B t u}{R}
$$

## ISENTROPIC PROCESSES

## Isentropic Processes

- The entropy of a fixed mass can be changed by: - Heat Transfer
$\square$ Irreversibilities
- Entropy of a fixed mass does not change during a process that is internally reversible and adiabatic. During this process entropy remains constant and we call it isentropic process

$$
\Delta s=0 \text { or } s_{2}=s_{1} \quad\left(\frac{k J}{k g-K)}\right.
$$



## Isentropic Processes

- A substance will have the same entropy value at the end of the process as it does the beginning if the process is carried out in an isentropic manner
- Many engineering systems or devices such as pumps, turbines, nozzles, and diffusers are essentially adiabatic in their operation, and they perform best when the irreversibilities are minimized (idealized conditions)


## Isentropic Processes

- A reversible adiabatic process is necessarily isentropic ( $s_{1}=$ $s_{2}$ ), but an isentropic process is not necessarily a reversible adiabatic process (the entropy increase of a substance during a process as a result of irreversibilities may be offset by a decrease in entropy as a result of heat losses, for example)
- The term isentropic process is customarily used in thermodynamics to imply an internally reversible, adiabatic process


## CLASS ACTIVITY

## Class Activity

- Steam enters an adiabatic turbine at 5 MPa and $450^{\circ} \mathrm{C}$ and leaves at a pressure of 1.4 MPa. Determine the work output of the turbine per unit mass of steam if the process is reversible.


## Class Activity

- Solutions (assumptions):
$\square$ This is a steady flow process (no change with respect to time), meaning $\Delta m_{C V}=0, \Delta E_{C V}=0, \Delta S_{C V}=0$ )
$\square$ The kinetic and potential energy changes are negligible $(\triangle K E=\triangle P E=0)$
$\square$ The process is adiabatic and thus there is no heat transfer
$\square$ The process is reversible



## Class Activity

- Solutions (processes):



## Class Activity

- Solutions (calculations):

$$
\begin{aligned}
& \dot{m}=\dot{m}_{1}=\dot{m}_{2} \\
& \dot{E}_{\text {in }}-\dot{E}_{\text {out }}=\frac{d E_{\text {system }}}{d t}=0 \\
& \dot{E}_{\text {in }}=\dot{E}_{\text {out }} \\
& \dot{m} h_{1}=\dot{W}_{\text {out }}+\dot{m} h_{2} \quad(\operatorname{since} \dot{Q}=0, k e \cong 0, p e \cong 0) \\
& \dot{W}_{\text {out }}=\dot{m}\left(h_{1}-h_{2}\right)
\end{aligned}
$$

## Class Activity

- Solutions (calculations):

$$
\dot{W}_{o u t}=h_{1}-h_{2}=3317.2-2967.4=349.8 \frac{\mathrm{~kJ}}{\mathrm{~kg}}
$$

$$
\begin{aligned}
& \left\{\begin{array}{lll} 
& & h_{1}=3317.2 \frac{\mathrm{~kJ}}{\mathrm{~kg}} \\
P_{1}=5 \mathrm{MPa} \\
T_{1}=450{ }^{\circ} \mathrm{C} & \rightarrow & s_{1}=6.8210 \frac{\mathrm{~kJ}}{\mathrm{~kg}-\mathrm{K}}
\end{array}\right. \\
& \left\{\begin{array}{c}
P_{2}=1.4 \mathrm{MPa} \\
s_{2}=s_{1}
\end{array} \quad \rightarrow \quad h_{2}=2967.4 \frac{\mathrm{~kJ}}{\mathrm{~kg}}\right.
\end{aligned}
$$

## PROPERTY DIAGRAMS INVOLVING ENTROPY

## Property Diagrams Involving Entropy

- Property diagrams serve as great visual aids in the thermodynamic analysis of processes
- Based on the $2^{\text {nd }}$ law, we can plot new diagrams that involve entropy:
Temperature-entropy
- Enthalpy-entropy


## Property Diagrams Involving Entropy

- We can rearrange our entropy equation:

$$
\delta Q_{i n t, r e v}=T d S
$$

$$
Q_{\text {int }, \text { rev }}=\int_{1}^{2} T d S \quad(k J)
$$


(The area under the process curve on a T-S diagram represents heat transfer during an internally reversible process)

## Property Diagrams Involving Entropy

- We can use the per-unit mass equation:

$$
\begin{equation*}
\delta q_{i n t, r e v}=T d s \tag{kJ}
\end{equation*}
$$

$$
q_{i n t, r e v}=\int_{1}^{2} T d s
$$


(The area under the process curve on a T-S diagram represents heat transfer during an internally reversible process)

## Property Diagrams Involving Entropy

- One special case (internally reversible isothermal process):

$$
Q_{\text {int }, \text { rev }}=T_{0} \Delta S
$$

$$
q_{i n t, r e v}=T_{0} \Delta s
$$

## Property Diagrams Involving Entropy

- T-s diagram for an isentropic process:



## Property Diagrams Involving Entropy

- h-s diagram (could be helpful for steady flow of devices such as nozzles, compressors, turbines):



## Property Diagrams Involving Entropy

- T-s diagram of water is given in the appendix:

Figure A-9


## Property Diagrams Involving Entropy

- h-s diagram of steam is given in the appendix:



## CLASS ACTIVITY

## Class Activity

- Show the Carnot cycle on a T-S diagram and indicate the areas that represent the heat supplied and rejected and the network in the diagram.


## Class Activity

- Solution:



## WHAT IS ENTROPY

## What Is Entropy

- Entropy can be viewed as a measure of molecular disorder or molecular randomness (lowest in solid phase and highest in the gas phase)



## What Is Entropy

- Oscillations in solid phase fade as temperature is decreased, and the molecules supposedly become motionless at absolute zero. This represents a state of ultimate molecular order (and minimum energy).
- The entropy of a pure crystalline substance at absolute zero temperature is zero since there is no uncertainty about the state of the molecules at that instant (3rd law of thermodynamics)



## What Is Entropy

- The third law of thermodynamics provide an absolute reference point for the determination of entropy
- The entropy determined relative to this point is called absolute entropy and it is extremely useful in the thermodynamics analysis of entropy
- The entropy of a substance that is not pure crystalline (such as a solid solution) is not zero at absolute zero temperature


## What Is Entropy

- A few examples:



## THE T DS RELATIONS

## The T ds Relations

- The first T ds (or Gibbs) equation (closed stationary system):

$$
\begin{align*}
& \delta Q_{i n t, r e v}-\delta W_{i n t, r e v, o u t}=d U \\
& T d S=d U+P d V  \tag{kJ}\\
& \delta Q_{i n t, r e v}=T d s \\
& T d s=d u+P d v \quad\left(\frac{k J}{k g}\right) \\
& \delta W_{\text {int }, \text { rev }, \text { out }}=P d V \\
& \left.\begin{array}{l}
T d s=d u+P d v \\
h=u+P v \rightarrow d h=d u+P d v+v d P
\end{array}\right\} \rightarrow T d s=d h-v d P
\end{align*}
$$

## The T ds Relations

- Use the first T ds (or Gibbs) equation to solve for entropy changes

$$
\begin{aligned}
& d s=\frac{d u}{T}+\frac{P d v}{T} \\
& d s=\frac{d u}{T}-\frac{v d P}{T}
\end{aligned}
$$



$$
\begin{aligned}
& T d s=d u+P d \cup \\
& T d s=d h-\cup d P
\end{aligned}
$$

## ENTROPY CHANGE OF LIQUIDS AND SOLIDS

## Entropy Change of Liquids and Solids

- Liquids and solids can be approximated as incompressible substances ( $d v \cong 0 \& c_{p}=c_{v}=c_{p}=c$ ):

$$
\begin{aligned}
& d s=\frac{d u}{T}-\frac{v d P}{T} \\
& s_{2}-s_{1}=\int_{1}^{2} c(T) \frac{d T}{T} \cong c_{\text {avg }} \ln \left(\frac{T_{2}}{T_{1}}\right) \\
& s_{2}-s_{1}=\int_{1}^{2} c(T) \frac{d T}{T} \cong c_{\text {avg }} \ln \left(\frac{T_{2}}{T_{1}}\right)=0 \quad \rightarrow \quad T_{2}=T_{1}
\end{aligned}
$$

(For isentropic)

## CLASS ACTIVITY

## Class Activity

- Liquid methane is commonly used in various cryogenic applications. The critical temperature of methane is 191 K (or ~ $82^{\circ} \mathrm{C}$ ) and thus methane must be maintained below 191 K to keep it in liquid phase. The properties of liquid methane at various temperature and pressure are given in Table below. Determine the entropy change of liquid methane as it undergoes a process from 110 K and 1 MPa to 120 K and 5 MPa .
a) Using tabulated properties
b) Approximating liquid methane as an incompressible substance?

| Properties of liquid methane |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| Temp., <br> $T, \mathrm{~K}$ | Pressure, <br> $P, \mathrm{MPa}$ | Density, <br> $\rho, \mathrm{kg} / \mathrm{m}^{3}$ | Enthalpy, <br> $h, \mathrm{~kJ} / \mathrm{kg}$ | Entropy, <br> $s, \mathrm{~kJ} / \mathrm{kg} \cdot \mathrm{K}$ | Specific heat, <br> $c_{p}, \mathrm{~kJ} / \mathrm{kg} \cdot \mathrm{K}$ |
| 110 | 0.5 | 425.3 | 208.3 | 4.878 | 3.476 |
|  | 1.0 | 425.8 | 209.0 | 4.875 | 3.471 |
|  | 2.0 | 426.6 | 210.5 | 4.867 | 3.460 |
|  | 5.0 | 429.1 | 215.0 | 4.844 | 3.432 |
| 120 | 410.4 | 243.4 | 5.185 | 3.551 |  |
|  | 1.0 | 411.0 | 244.1 | 5.180 | 3.543 |

## Class Activity

- Solutions (a):

$$
\begin{aligned}
& \left.\begin{array}{l}
P_{1}=1 \mathrm{MPa} \\
T_{1}=110 \mathrm{~K}
\end{array}\right\} \rightarrow \begin{array}{l}
s_{1}=4.875 \frac{\mathrm{~kJ}}{\mathrm{~kg}-\mathrm{K}} \\
c_{p 1}=3.471 \frac{\mathrm{~kJ}}{\mathrm{~kg}-\mathrm{K}}
\end{array} \\
& \left.\begin{array}{l}
P_{2}=5 M P a \\
T_{2}=120 \mathrm{~K}
\end{array}\right\} \rightarrow \begin{array}{l}
s_{1}=5.145 \frac{\mathrm{~kJ}}{\mathrm{~kg}-\mathrm{K}} \\
c_{p 1}=3.486 \frac{\mathrm{~kJ}}{\mathrm{~kg}-\mathrm{K}}
\end{array}
\end{aligned}
$$



$$
\Delta s=s_{2}-s_{1}=5.145-4.875=0.270 \frac{k J}{k g-K}
$$

## Class Activity

- Solutions (b):

$$
\begin{aligned}
c_{a v g} & =\frac{c_{p 1}+c_{p 2}}{2}=\frac{3.471+3.486}{2}=3.4785 \frac{\mathrm{~kJ}}{\mathrm{~kg}-\mathrm{K}} \\
\Delta s & =c_{a v g} \ln \left(\frac{T_{2}}{T_{1}}\right)=\left(3.4785 \frac{\mathrm{~kJ}}{\mathrm{~kg}-\mathrm{K}}\right) \operatorname{Ln}\left(\frac{120 \mathrm{~K}}{110 \mathrm{~K}}\right)=0.303 \frac{\mathrm{~kJ}}{\mathrm{~kg}-\mathrm{K}}
\end{aligned}
$$

## Class Activity

- Solutions (error):

$$
\text { Error }=\frac{\Delta s_{\text {actual }}-\Delta_{\text {ideal }}}{\Delta s_{\text {actual }}}=\frac{|0.27-0.303|}{0.270}=0.122(\text { or } 12.2 \%)
$$

