CAE 208 / MMAE 320: Thermodynamics Fall 2023

October 5, 2023 Energy analysis of closed systems (2)

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ANNOUNCEMENTS

Announcement



LUNCH WITH ARCHITECTURAL ENGINEERING PROFESSORS

Are you interested in building systems? Join us to discuss HVAC, lighting fixtures, and building design. Open to any major!

Q	Location: AM 120
	Date: October 12
()	Time: 12:45 - 1:40
WP	Food is Provided!!

For more information, feel free to email ashrae_iit@iit.edu or send a Instagram dm to @ashrae_iit.

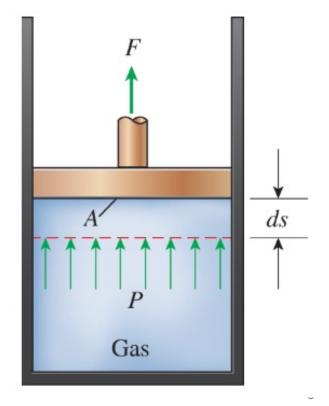
Announcements

- Midterm is scheduled for October 10:
 - The first part of the exam is closed book (You are allowed to have one page for your cheat sheet to include equations)
 - □ The second part of the exam is open book (only a thermodynamics book or thermodynamics property tables)

RECAP

 The expansion or compression work is often called moving boundary work or simply boundary work

 $\delta W_b = Fds = PAds = P dV$



• For a quasi-equilibrium expansion process, we can write:

$$Area = A = \int_{1}^{2} dA = \int_{1}^{2} P dV$$

$$W_{b} = \int_{1}^{2} P_{i} dV$$

$$Process path$$

$$W_{b} = \int_{1}^{2} P_{i} dV$$

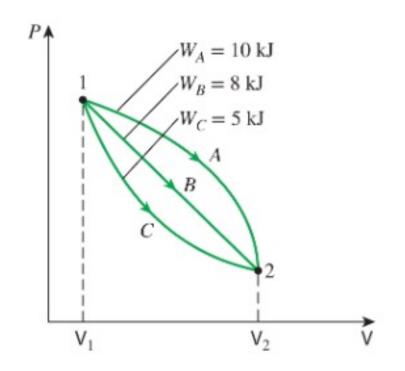
$$W_{b} = \int_{1}^{2} P_{i} dV$$

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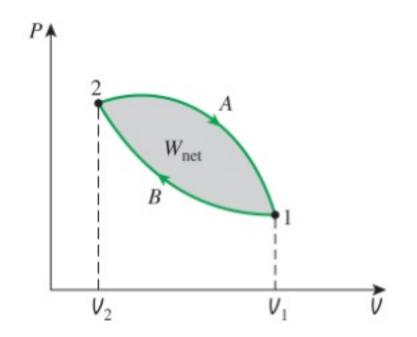
• For a quasi-equilibrium expansion process, we can write:

$$W_b = \int_1^2 P_i dV$$

 The boundary work done during a process depends on the path followed as well as the end states:

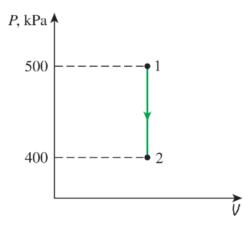


 The net work done during a cycle is the difference between the work done by the system and the work done on the system:

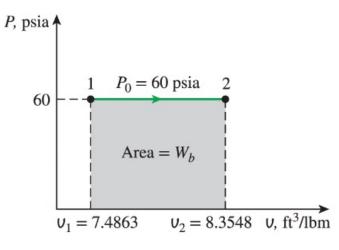


Recap

Constant Volume



Constant Pressure



QUIZ

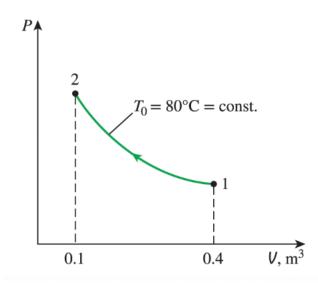
Quiz

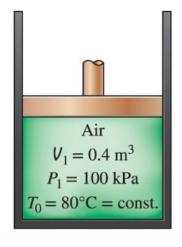
CLASS ACTIVITY

Class Activity

A piston-cylinder device initially contains 0.4 m³ of air at 100 kPa and 80 °C. The air is now compressed to 0.1 m³ in such a way that the temperature inside the cylinder remains constant. Determine the work done during this process

• Solution:

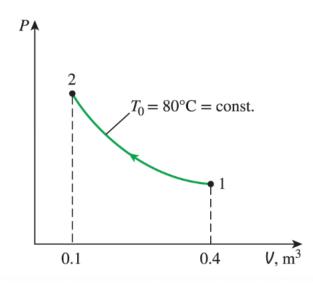




$$PV = mRT_0 \rightarrow P = \frac{C}{V}$$

$$W_{b} = \int_{1}^{2} P dV = \int_{1}^{2} (\frac{C}{V}) dV = C \int_{1}^{2} (\frac{dV}{V})$$

• Solution:

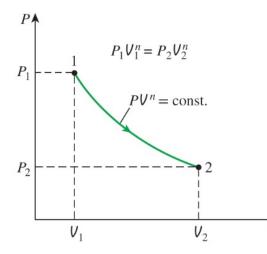


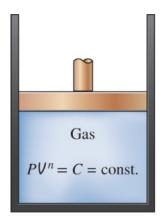
$$W_b = C \times Ln(V) \Big|_{V_1}^{V_2} = C[Ln(V_2) - Ln(V_1)] = P_1 V_1 \times Ln(\frac{V_2}{V_1})$$

$$W_b = (100 \ kPa)(0.4 \ m^3) \left(\ln\left(\frac{0.1}{0.4}\right) \right) \left(\frac{1kJ}{1 \ kPa. \ m^2}\right) = -55.5 \ kJ$$

 During expansion or compression processes of gases and volume are often related in PVⁿ = C which is known as a Polytropic process

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$$P = CV^{-n}$$

• Polytropic process

 $P = CV^{-n}$

$$W_b = \int_1^2 P \, dV = \int_1^2 (CV^{-n}) dV = \frac{C((V^{-n+1} - V^{-n+1}))}{(-n+1)} = \frac{P_2 V_2 - P_1 V_1}{1 - n}$$

• Polytropic process

 $C = P_1 V_1^n = P_2 V_2^n$

$$W_b = \frac{mR(T_2 - T_1)}{1 - n} \quad n \neq 1 \ (kJ)$$

• For the case of n =1

$$W_{b} = \int_{1}^{2} P dV = \int_{1}^{2} CV^{-1} dV = PV \times Ln(\frac{V_{2}}{V_{1}})$$

• Moving boundary work under different processes

Process	Moving boundary work
Constant volume	0
Constant pressure	$P_0(V_2-V_1)$
Isothermal	$P_{1}V_{1} \times Ln(\frac{V_{2}}{V_{1}})$ $P_{1}V_{1} \times Ln(\frac{P_{1}}{P_{2}})$ $mRT_{o} \times Ln(\frac{V_{2}}{V_{1}})$
Polytropic	$\frac{\frac{P_2V_2 - P_1V_1}{1 - n}}{\frac{mR(T_2 - T_1)}{1 - n}}$

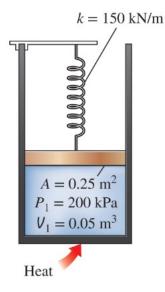
CLASS ACTIVITY

Class Activity

- A piston-cylinder device contains 0.05 m³ of a gas initially at 200 kPa. At this state, a linear spring that has a spring constant of 150 kN/m is touching the piston but exerting no force on it. Now heat is transferred to the gas, causing the piston to rise and to compress the spring until the volume inside the cylinder doubles. If the cross-sectional area of the piston is 0.25 m², determine
 - a) The final pressure inside the cylinder
 - b) The total work done by the gas
 - c) The fraction of this work done against the spring to compress it

Class Activity

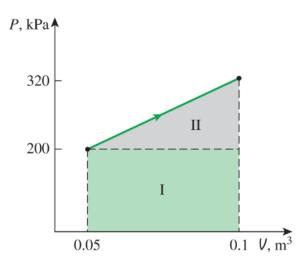
• Solution



$$V_2 = 2V_1 = 2(0.05 m^3) = 0.1 m^3$$

$$x = \frac{\Delta V}{A} = \frac{(0.1 - 0.05)m^3}{0.25 m^2} = 0.2 m$$

• Solution

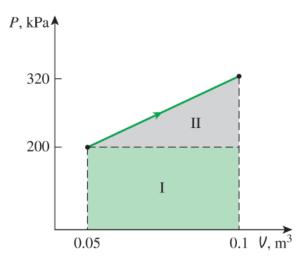


$$F = kx = \left(150\frac{kN}{m}\right)(0.2\ m) = 30\ kN$$

$$P = \frac{F}{A} = \frac{30 \ kN}{0.25 \ m^2} = 120 \ kN$$

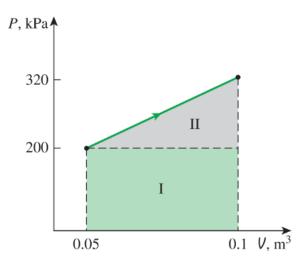
 $200 + 120 = 320 \ kN$

• Solution (b)



$$W = area = \frac{(200 + 320)kPa}{2} [0.1^2 - 0.05^2] \left(\frac{1kJ}{1 \ kPa. \ m^2}\right) = 13 \ kJ$$

• Solution (c)



$$W_{spring} = \frac{1}{2} [320 - 200] kPa(0.05 \ m^3) = 3 \ kJ$$

$$W_{spring} = \frac{1}{2}k(x_2^2 - x_1^2) = \frac{1}{2}(150)(0.2^2 - 0^2) = 3 kJ$$

ENERGY BALANCE FOR CLOSED SYSTEMS

 The net change (increase or decrease) in the total energy of the system during a process is equal to the difference between the total energy entering and the total energy leaving the system during the process

(Total energy entering the system) – (Total energy leaving the system) = (Change in the total energy of the sysem)

$$E_{in} - E_{out} = \Delta E_{system}$$

This is known as the energy balance

• Energy change of a system ΔE_{system}

Energy change = Energy at final state - Energy at initial state

$$\Delta E_{system} = E_{final} - E_{initial} = E_2 - E_1$$

Energy is a property, and the value of a property does not change unless the state of the system changes

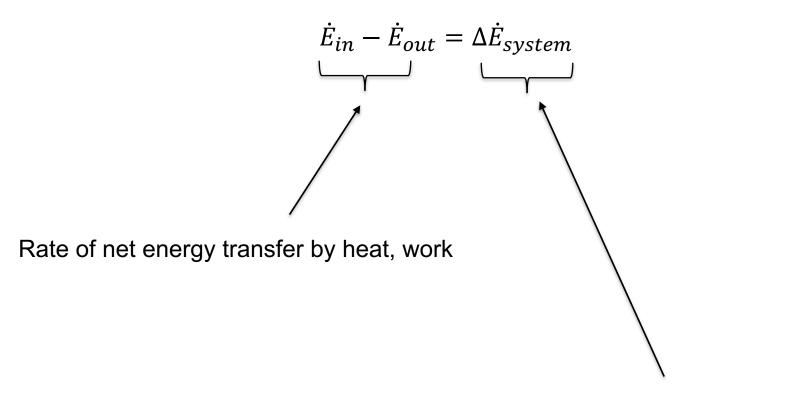
• We can sum the heat, work, and mass, and the heat transfer:

$$E_{in} - E_{out} = (Q_{in} - Q_{out}) + (W_{in} - W_{out}) = \Delta E_{system}$$

Net energy transfer by heat, work

Change in internal, kinetic, potential, ..., energies

 We can sum the heat, work, and mass, and the heat transfer in the rate form:



Rate of change in internal, kinetic, potential, ..., energies

 The energy balance can be expressed on a per unit mass basis as

 $e_{in} - e_{out} = \Delta e_{system}$

• For constant rates, we can write:

$$Q = \dot{Q} \Delta t$$

 $W = \dot{W} \Delta t$

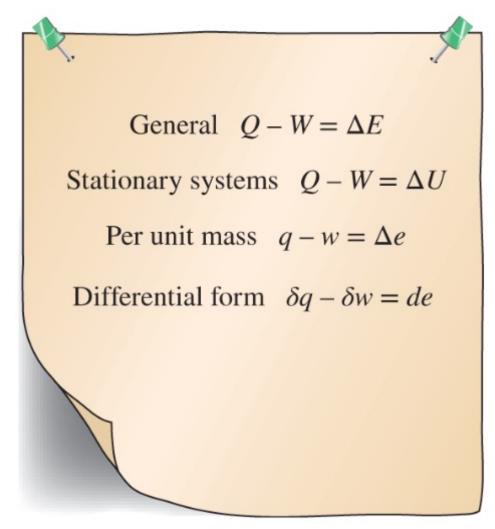
$$E = \left(\frac{dE}{dt}\right)\Delta t$$

 For a closed system undergoing a cycle, the initial and final states are identical:

V

Energy Balance for Closed Systems

• We can write:



CLASS ACTIVITY

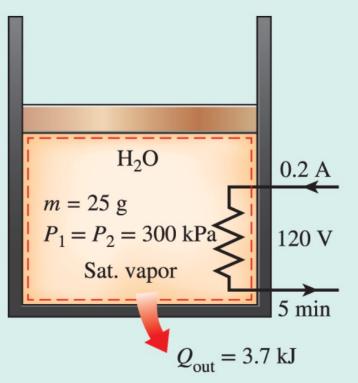
Class Activity

- A piston-cylinder device contains 25 g of saturated vapor that is maintained at a constant pressure of 300 kPa. A resistance heater within the cylinder is turned on and passes a current of 0.2 A for 5 min from a 120-V source. At the same time, a heat loss of 3.7 kJ occurs.
 - a) Show that for a closed system the boundary work W_b and the change in internal energy ΔU in the first-law relation can be contained into one term ΔH for a constant pressure process
 - b) Determine the final temperature of the system

$$E_{in} - E_{out} = \Delta E_{system}$$

$$Q - W = \Delta U + \Delta KE + \Delta PE$$

$$Q - W_{other} - W_b = U_2 - U_1$$



$$W_b = P_0(V_2 - V_1)$$

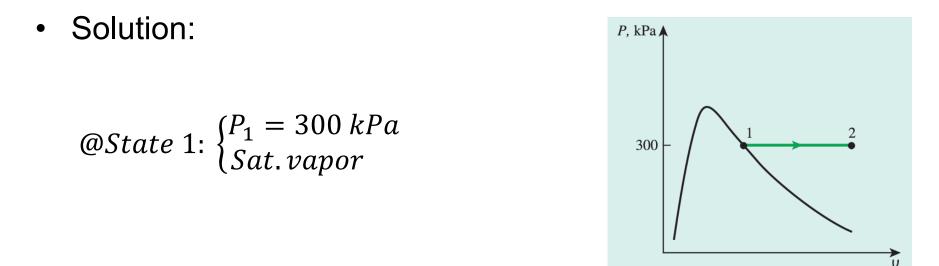
$$Q - W_{other} - P_0(V_2 - V_1) = U_2 - U_1$$

 $P_0 = P_2 = P_1$

$$Q - W_{other} = (U_2 + P_2 V_2) - (U_1 + P_1 V_1)$$

 $Q - W_{other} = H_2 - H_1$

Class Activity



APPENDIX 1

PROPERTY TABLES AND CHARTS (SI UNITS)

- 🕑 TABLE A-1
 - **_E A–1** Molar mass, gas constant, and critical-point properties 852
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Class Activity

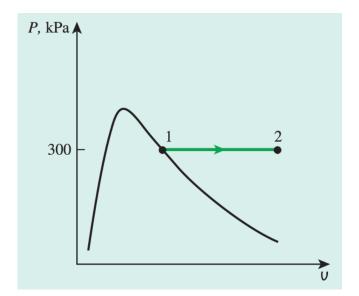
• Solution:

TABLE A-5

Saturated water—Pressure table

Press., <i>P</i> kPa	Sat. temp., T _{sat} °C	<i>Specific volume,</i> m ³ /kg		Internal energy, kJ/kg			Enthalpy, kJ/kg		
		Sat. liquid, U _f	Sat. vapor, v _g	Sat. liquid, <i>u_f</i>	Evap., <i>u_{fg}</i>	Sat. vapor, u _g	Sat. liquid, <i>h_f</i>	Evap., h _{fg}	Sat. vapor, h _g
275	130.58	0.001070	0.65732	548.57	1991.6	2540.1	548.86	2172.0	2720.9
300	133.52	0.001073	0.60582	561.11	1982.1	2543.2	561.43	2163.5	2724.9
325	136.27	0.001076	0.56199	572.84	1973.1	2545.9	573.19	2155.4	2728.6
350	138.86	0.001079	0.52422	583.89	1964.6	2548.5	584.26	2147.7	2732.0

@State 1:
$$\begin{cases} P_1 = 300 \ kPa \\ Sat. \ vapor \end{cases} \quad h_1 = h_{g \ @300 \ kPa} = 2724.9 \frac{kJ}{kg}$$



• Solution (b):

$$W_e = VI\Delta t = (120 V)(0.2 A)(300 s) \left(\frac{1\frac{kJ}{s}}{1000 VA}\right) = 7.2 kJ$$

Class Activity

• Solution (b):

$$E_{in} - E_{out} = \Delta E_{system}$$

$$W_{e,in} - Q_{out} - W_b = \Delta U$$

$$W_{e,in} - Q_{out} = \Delta \mathbf{H} = \mathbf{m}(\mathbf{h}_2 - \mathbf{h}_1)$$

• Solution (b):

 $7.2 kJ - 3.7 kJ = (0.025 kg)(h_2 - 2724.9) kJ/kg$

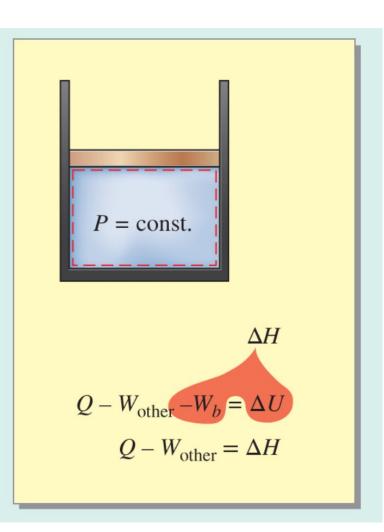
$$h_2 = 2864.9 \frac{kJ}{kg}$$

• Solution (b):

$$\begin{cases} P_2 = 300 \, kPa \\ h_2 = 2865.9 \frac{kJ}{kg} & T_2 = 200 \,^{\circ}C \end{cases}$$

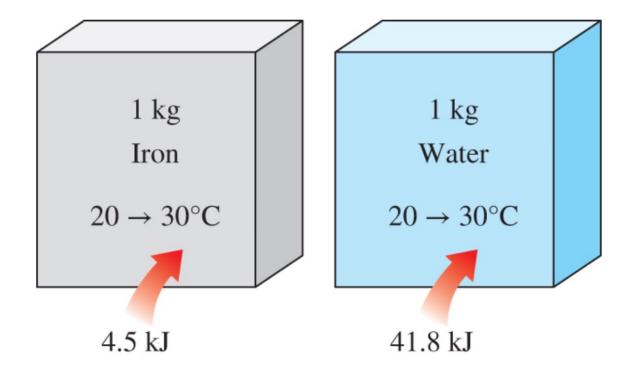
TABLE A-6													
Superheated water													
T °C	v m ³ /kg	<i>u</i> kJ/kg	h kJ/kg	s kJ/kg ∙ K	u m ³ /kg	u kJ/kg	<i>h</i> kJ/kg	s kJ/kg ∙ K					
	I	P = 0.01 MI	Pa (45.81°	°C)*	$P = 0.05 \text{ MPa} (81.32^{\circ}\text{C})$								
		P = 0.20 M	Pa (120.2	21°C)	$P = 0.30 \text{ MPa} (133.52^{\circ}\text{C})$								
Sat.	0.88578	2529.1	2706.3	7.1270	0.60582	2543.2	2724.9	6.9917					
150	0.95986	2577.1	2769.1	7.2810	0.63402	2571.0	2761.2	7.0792					
200	1.08049	2654.6	2870.7	7.5081	0.71643	2651.0	2865.9	7.3132					
250	1.19890	2731.4	2971.2	7.7100	0.79645	2728.9	2967.9	7.5180					
300	1.31623	2808.8	3072.1	7.8941	0.87535	2807.0	3069.6	7.7037					
400	1.54934	2967.2	3277.0	8.2236	1.03155	2966.0	3275.5	8.0347					
500	1.78142	3131.4	3487.7	8.5153	1.18672	3130.6	3486.6	8.3271					

• Summary:

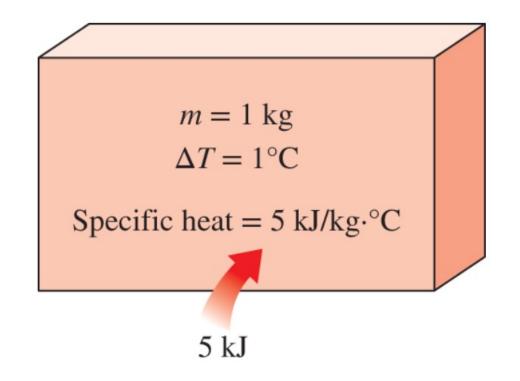


SPECIFIC HEATS

 How much heat do we need to add to increase temperature of 1 kg iron vs water for 10 °C?



• Specific heat is defined as the energy required to raise temperature of a unit mass of substance by one degree

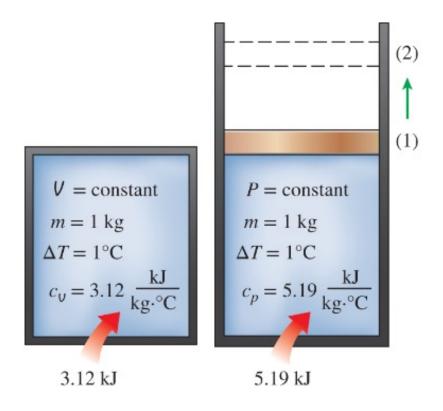


Specific Heats

- Specific heat is defined as the energy required to raise temperature of a unit mass of substance by one degree
 - \Box Specific heat at constant volume (c_v)
 - \Box Specific heat at constant pressure (c_p)

Specific Heats

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 - \Box Specific heat at constant volume (c_v)
 - \Box Specific heat at constant pressure (c_p)



 Let's start from the fixed mass in a stationary closed system that undergoes a constant volume process:

$$\delta e_{in} - \delta e_{out} = dU + dKE + dPE = \delta Q - \delta W$$

$$\delta Q = dU + \delta W = dU + PdV$$

$$c_{v} = \frac{1}{m} \left(\frac{\delta Q}{\delta T} \right)_{v} = \frac{1}{m} \left(\frac{\partial U}{\partial T} \right)_{v} = \left(\frac{\partial u}{\partial T} \right)_{v}$$

 $c_{v}dT = du$

Specific Heats

Similarly, we can write the following for a constant pressure process:

$$\delta Q = dU + \delta W = dU + PdV$$

$$c_p = \frac{1}{m} \left(\frac{\delta Q}{\delta T} \right)_p = \frac{1}{m} \left(\frac{\partial H}{\partial T} \right)_p = \left(\frac{\partial h}{\partial T} \right)_p$$

$$c_p = \left(\frac{\partial h}{\partial T}\right)_p$$

Specific Heats

