## CAE 208 / MMAE 320: Thermodynamics Fall 2023

## October 5, 2023 <br> Energy analysis of closed systems (2)

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## ANNOUNCEMENTS

## Announcement



## LUNCH WITH ARCHITECTURAL ENGINEERING PROFESSORS

Are you interested in building systems? Join us to discuss HVAC, lighting fixtures, and building design.

Open to any major!

P Location: AM 120<br>ixi<br>() Time: 12:45-1:40<br>\$ Food is Provided!!

For more information, feel free to email ashrae_iiteiit.edu or send a

## Announcements

- Midterm is scheduled for October 10:

The first part of the exam is closed book (You are allowed to have one page for your cheat sheet to include equations)
The second part of the exam is open book (only a thermodynamics book or thermodynamics property tables)

RECAP

## Recap

- The expansion or compression work is often called moving boundary work or simply boundary work

$$
\delta W_{b}=F d s=P A d s=P d V
$$



## Recap

- For a quasi-equilibrium expansion process, we can write:

$$
\begin{aligned}
& \text { Area }=A=\int_{1}^{2} d A=\int_{1}^{2} P d V \\
& W_{b}=\int_{1}^{2} P_{i} d V
\end{aligned}
$$



## Recap

- For a quasi-equilibrium expansion process, we can write:

$$
W_{b}=\int_{1}^{2} P_{i} d V
$$

## Recap

- The boundary work done during a process depends on the path followed as well as the end states:



## Recap

- The net work done during a cycle is the difference between the work done by the system and the work done on the system:



## Recap

- Constant Volume

- Constant Pressure


QUIZ

## Quiz

## CLASS ACTIVITY

## Class Activity

- A piston-cylinder device initially contains $0.4 \mathrm{~m}^{3}$ of air at 100 kPa and $80^{\circ} \mathrm{C}$. The air is now compressed to $0.1 \mathrm{~m}^{3}$ in such a way that the temperature inside the cylinder remains constant. Determine the work done during this process


## Class Activity

- Solution:



$$
P V=m R T_{0} \rightarrow P=\frac{C}{V}
$$

$$
W_{b}=\int_{1}^{2} P d V=\int_{1}^{2}\left(\frac{C}{V}\right) d V=C \int_{1}^{2}\left(\frac{d V}{V}\right)
$$

## Class Activity

- Solution:


$$
W_{b}=(100 k P a)\left(0.4 m^{3}\right)\left(\operatorname{Ln}\left(\frac{0.1}{0.4}\right)\right)\left(\frac{1 k J}{1 k P a . m^{2}}\right)=-55.5 k J
$$

## Moving Boundary Work

- During expansion or compression processes of gases and volume are often related in $\mathrm{PV}^{\mathrm{n}}=\mathrm{C}$ which is known as a Polytropic process



$$
P=C V^{-n}
$$

## Moving Boundary Work

- Polytropic process

$$
\begin{aligned}
& P=C V^{-n} \\
& W_{b}=\int_{1}^{2} P d V=\int_{1}^{2}\left(C V^{-n}\right) d V=\frac{C\left(\left(V^{-n+1}-V^{-n+1}\right)\right.}{(-n+1)}=\frac{P_{2} V_{2}-P_{1} V_{1}}{1-n}
\end{aligned}
$$

## Moving Boundary Work

- Polytropic process

$$
\begin{aligned}
& C=P_{1} V_{1}^{n}=P_{2} V_{2}^{n} \\
& W_{b}=\frac{m R\left(T_{2}-T_{1}\right)}{1-n} \quad n \neq 1(k J)
\end{aligned}
$$

## Moving Boundary Work

- For the case of $\mathrm{n}=1$

$$
W_{b}=\int_{1}^{2} P d V=\int_{1}^{2} C V^{-1} d V=P V \times \operatorname{Ln}\left(\frac{V_{2}}{V_{1}}\right)
$$

## Moving Boundary Work

- Moving boundary work under different processes

| Process | Moving boundary work |
| :--- | :---: |
| Constant volume | 0 |
| Constant pressure | $P_{0}\left(V_{2}-V_{1}\right)$ |
| Isothermal | $P_{1} V_{1} \times \operatorname{Ln}\left(\frac{V_{2}}{V_{1}}\right)$ |
|  | $P_{1} V_{1} \times \operatorname{Ln}\left(\frac{P_{1}}{P_{2}}\right)$ |
|  | $m R T_{o} \times \operatorname{Ln}\left(\frac{V_{2}}{V_{1}}\right)$ |
| Polytropic | $\frac{P_{2} V_{2}-P_{1} V_{1}}{1-n}$ |
|  | $\frac{m R\left(T_{2}-T_{1}\right)}{1-n}$ |

## CLASS ACTIVITY

## Class Activity

- A piston-cylinder device contains $0.05 \mathrm{~m}^{3}$ of a gas initially at 200 kPa . At this state, a linear spring that has a spring constant of $150 \mathrm{kN} / \mathrm{m}$ is touching the piston but exerting no force on it. Now heat is transferred to the gas, causing the piston to rise and to compress the spring until the volume inside the cylinder doubles. If the cross-sectional area of the piston is $0.25 \mathrm{~m}^{2}$, determine
a) The final pressure inside the cylinder
b) The total work done by the gas
c) The fraction of this work done against the spring to compress it


## Class Activity

- Solution


$$
\begin{aligned}
& V_{2}=2 V_{1}=2\left(0.05 \mathrm{~m}^{3}\right)=0.1 \mathrm{~m}^{3} \\
& x=\frac{\Delta V}{A}=\frac{(0.1-0.05) \mathrm{m}^{3}}{0.25 \mathrm{~m}^{2}}=0.2 \mathrm{~m}
\end{aligned}
$$

## Class Activity

- Solution

$$
\begin{aligned}
& P, \mathrm{kPa} \\
& F=k x=\left(150 \frac{\mathrm{kN}}{\mathrm{~m}}\right)(0.2 \mathrm{~m})=30 \mathrm{kN} \\
& P=\frac{F}{A}=\frac{30 \mathrm{kN}}{0.25 \mathrm{~m}^{2}}=120 \mathrm{kN}
\end{aligned}
$$

$$
200+120=320 k N
$$

## Class Activity

- Solution (b)


$$
W=\text { area }=\frac{(200+320) k P a}{2}\left[0.1^{2}-0.05^{2}\right]\left(\frac{1 k J}{1 k P a . m^{2}}\right)=13 k J
$$

## Class Activity

- Solution (c)


$$
W_{\text {spring }}=\frac{1}{2}[320-200] k P a\left(0.05 m^{3}\right)=3 k J
$$

$$
W_{\text {spring }}=\frac{1}{2} k\left(x_{2}^{2}-x_{1}^{2}\right)=\frac{1}{2}(150)\left(0.2^{2}-0^{2}\right)=3 k J
$$

## ENERGY BALANCE FOR CLOSED SYSTEMS

## Energy Balance for Closed Systems

- The net change (increase or decrease) in the total energy of the system during a process is equal to the difference between the total energy entering and the total energy leaving the system during the process
(Total energy entering the system) - (Total energy leaving the system) $=$ (Change in the total energy of the sysem)

$$
E_{\text {in }}-E_{\text {out }}=\Delta E_{\text {system }}
$$

## Energy Balance for Closed Systems

- Energy change of a system $\Delta E_{\text {system }}$

$$
\begin{aligned}
& \text { Energy change }=\text { Energy at final state }- \text { Energy at initial state } \\
& \qquad \Delta E_{\text {system }}=E_{\text {final }}-E_{\text {initial }}=E_{2}-E_{1}
\end{aligned}
$$

Energy is a property, and the value of a property does not change unless the state of the system changes

## Energy Balance for Closed Systems

- We can sum the heat, work, and mass, and the heat transfer:

$$
E_{\text {in }}-E_{\text {out }}=\left(Q_{\text {in }}-Q_{\text {out }}\right)+\left(W_{\text {in }}-W_{\text {out }}\right)=\Delta E_{\text {system }}
$$



Net energy transfer by heat, work

Change in internal, kinetic, potential, ..., energies

## Energy Balance for Closed Systems

- We can sum the heat, work, and mass, and the heat transfer in the rate form:


Rate of change in internal, kinetic, potential, ..., energies

## Energy Balance for Closed Systems

- The energy balance can be expressed on a per unit mass basis as

$$
e_{\text {in }}-e_{\text {out }}=\Delta e_{\text {system }}
$$

## Energy Balance for Closed Systems

- For constant rates, we can write:

$$
Q=\dot{Q} \Delta t
$$

$$
W=\dot{W} \Delta t
$$

$$
E=\left(\frac{d E}{d t}\right) \Delta t
$$

## Energy Balance for Closed Systems

- For a closed system undergoing a cycle, the initial and final states are identical:

$$
\begin{aligned}
& \Delta E=E_{\text {in }}-E_{\text {out }}=0 \rightarrow E_{\text {in }}=E_{\text {out }} \\
& W_{\text {net,out }}=Q_{n e t, \text { in }} \rightarrow \dot{W}_{n e t, o u t}=\dot{Q}_{n e t, i n}
\end{aligned}
$$



## Energy Balance for Closed Systems

- We can write:



## CLASS ACTIVITY

## Class Activity

- A piston-cylinder device contains 25 g of saturated vapor that is maintained at a constant pressure of 300 kPa . A resistance heater within the cylinder is turned on and passes a current of 0.2 A for 5 min from a $120-\mathrm{V}$ source. At the same time, a heat loss of 3.7 kJ occurs.
a) Show that for a closed system the boundary work $\mathrm{W}_{\mathrm{b}}$ and the change in internal energy $\Delta U$ in the first-law relation can be contained into one term $\Delta H$ for a constant pressure process
b) Determine the final temperature of the system


## Class Activity

- Solution:

$$
\begin{aligned}
& E_{\text {in }}-E_{\text {out }}=\Delta E_{\text {system }} \\
& Q-W=\Delta U+\Delta K E+\Delta P E \\
& Q-W_{\text {other }}-W_{b}=U_{2}-U_{1}
\end{aligned}
$$



## Class Activity

- Solution:

$$
\begin{aligned}
& W_{b}=P_{0}\left(V_{2}-V_{1}\right) \\
& Q-W_{\text {other }}-P_{0}\left(V_{2}-V_{1}\right)=U_{2}-U_{1}
\end{aligned}
$$

## Class Activity

- Solution:

$$
\begin{aligned}
& P_{0}=P_{2}=P_{1} \\
& Q-W_{\text {other }}=\left(U_{2}+P_{2} V_{2}\right)-\left(U_{1}+P_{1} V_{1}\right) \\
& Q-W_{\text {other }}=H_{2}-H_{1}
\end{aligned}
$$

## Class Activity

- Solution:

$$
\text { @State 1: }\left\{\begin{array}{l}
P_{1}=300 \mathrm{kPa} \\
\text { Sat.vapor }
\end{array}\right.
$$



## APPENDIX 1

## PROPERTY TABLES AND CHARTS (SI UNITS)

| TABLE A-1 | Molar mass, gas constant, and critical-point properties 852 |
| :--- | :--- |
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## Class Activity

## - Solution:

| TABLE A-5 |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Saturated water-Pressure table |  |  |  |  |  |  |  |  |  |
|  | Sat. | Specific volume,$\mathrm{m}^{3} / \mathrm{kg}$ |  | Internal energy, <br> kJ/kg |  |  | Enthalpy, <br> kJ/kg |  |  |
| $P \mathrm{kPa}$ | $\begin{aligned} & \text { temp., } \\ & T_{\text {sat }}{ }^{\circ} \mathrm{C} \end{aligned}$ | Sat. <br> liquid, $v_{f}$ | Sat. <br> vapor, $v_{g}$ | Sat. liquid, $u_{f}$ | $\begin{aligned} & \text { Evap., } \\ & u_{f g} \end{aligned}$ | Sat. <br> vapor, <br> $u_{g}$ | Sat. <br> liquid, <br> $h_{f}$ | Evap., $h_{f g}$ | Sat. <br> vapor, <br> $h_{g}$ |
| 275 | 130.58 | 0.001070 | 0.65732 | 548.57 | 1991.6 | 2540.1 | 548.86 | 2172.0 | 2720.9 |
| 300 | 133.52 | 0.001073 | 0.60582 | 561.11 | 1982.1 | 2543.2 | 561.43 | 2163.5 | 2724.9 |
| 325 | 136.27 | 0.001076 | 0.56199 | 572.84 | 1973.1 | 2545.9 | 573.19 | 2155.4 | 2728.6 |
| 350 | 138.86 | 0.001079 | 0.52422 | 583.89 | 1964.6 | 2548.5 | 584.26 | 2147.7 | 2732.0 |

## Class Activity

- Solution:

$$
\text { @State 1: }\left\{\begin{array}{l}
P_{1}=300 \mathrm{kPa} \\
\text { Sat.vapor }
\end{array} \quad h_{1}=h_{g} @ 300 \mathrm{kPa}=2724.9 \frac{\mathrm{~kJ}}{\mathrm{~kg}}\right.
$$



## Class Activity

- Solution (b):

$$
W_{e}=V I \Delta t=(120 V)(0.2 A)(300 s)\left(\frac{1 \frac{k J}{s}}{1000 V A}\right)=7.2 \mathrm{~kJ}
$$

## Class Activity

- Solution (b):

$$
\begin{gathered}
E_{\text {in }}-E_{\text {out }}=\Delta E_{\text {system }} \\
W_{e, \text { in }}-Q_{\text {out }}-W_{b}=\Delta U \\
W_{e, \text { in }}-Q_{\text {out }}=\Delta \mathrm{H}=\mathrm{m}\left(\mathrm{~h}_{2}-\mathrm{h}_{1}\right)
\end{gathered}
$$

## Class Activity

- Solution (b):

$$
\begin{aligned}
7.2 \mathrm{~kJ}-3.7 \mathrm{~kJ} & =(0.025 \mathrm{~kg})\left(\mathrm{h}_{2}-2724.9\right) \mathrm{kJ} / \mathrm{kg} \\
h_{2} & =2864.9 \frac{\mathrm{~kJ}}{\mathrm{~kg}}
\end{aligned}
$$

## Class Activity

- Solution (b):

$$
\left\{\begin{array}{l}
P_{2}=300 k P a \\
h_{2}=2865.9 \frac{\mathrm{~kJ}}{\mathrm{~kg}}
\end{array} \quad \mathrm{~T}_{2}=200^{\circ} \mathrm{C}\right.
$$

| TABLE A-6 |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Superheated water |  |  |  |  |  |  |  |  |
| $\begin{aligned} & T \\ & { }^{\circ} \mathrm{C} \end{aligned}$ | $\mathrm{m}^{3} / \mathrm{kg}$ | kJ/kg | $\begin{aligned} & h \\ & \mathrm{~kJ} / \mathrm{kg} \end{aligned}$ | $\mathrm{kJ} / \mathrm{kg} \cdot \mathrm{~K}$ | $\mathrm{m}^{3} / \mathrm{kg}$ | $\mathrm{kJ} / \mathrm{kg}$ | $\begin{aligned} & h \\ & \mathrm{~kJ} / \mathrm{kg} \end{aligned}$ | $\mathrm{kJ} / \mathrm{kg} \cdot \mathrm{~K}$ |
| $P=0.01 \mathrm{MPa}\left(45.81{ }^{\circ} \mathrm{C}\right)^{*}$ |  |  |  |  | $P=0.05 \mathrm{MPa}\left(81.32^{\circ} \mathrm{C}\right)$ |  |  |  |
|  | $P=0.20 \mathrm{MPa}\left(120.21^{\circ} \mathrm{C}\right)$ |  |  |  | $P=0.30 \mathrm{MPa}\left(133.52^{\circ} \mathrm{C}\right)$ |  |  |  |
| Sat. | 0.88578 | 2529.1 | 2706.3 | 7.1270 | 0.60582 | 2543.2 | 2724.9 | 6.9917 |
| 150 | 0.95986 | 2577.1 | 2769.1 | 7.2810 | 0.63402 | 2571.0 | 2761.2 | 7.0792 |
| 200 | 1.08049 | 2654.6 | 2870.7 | 7.5081 | 0.71643 | 2651.0 | 2865.9 | 7.3132 |
| 250 | 1.19890 | 2731.4 | 2971.2 | 7.7100 | 0.79645 | 2728.9 | 2967.9 | 7.5180 |
| 300 | 1.31623 | 2808.8 | 3072.1 | 7.8941 | 0.87535 | 2807.0 | 3069.6 | 7.7037 |
| 400 | 1.54934 | 2967.2 | 3277.0 | 8.2236 | 1.03155 | 2966.0 | 3275.5 | 8.0347 |
| 500 | 1.78142 | 3131.4 | 3487.7 | 8.5153 | 1.18672 | 3130.6 | 3486.6 | 8.3271 |

## Class Activity

- Summary:



## SPECIFIC HEATS

## Specific Heats

- How much heat do we need to add to increase temperature of 1 kg iron vs water for $10^{\circ} \mathrm{C}$ ?

4.5 kJ

41.8 kJ


## Specific Heats

- Specific heat is defined as the energy required to raise temperature of a unit mass of substance by one degree



## Specific Heats

- Specific heat is defined as the energy required to raise temperature of a unit mass of substance by one degree
$\square$ Specific heat at constant volume ( $c_{v}$ )
$\square$ Specific heat at constant pressure ( $\mathrm{c}_{\mathrm{p}}$ )


## Specific Heats

- Specific heat is defined as the energy required to raise temperature of a unit mass of substance by one degree
$\square$ Specific heat at constant volume ( $c_{v}$ )
$\square$ Specific heat at constant pressure ( $\mathrm{c}_{\mathrm{p}}$ )

3.12 kJ



## Specific Heats

- Let's start from the fixed mass in a stationary closed system that undergoes a constant volume process:

$$
\delta e_{i n}-\delta e_{o u t}=d U+d K E+d P E=\delta Q-\delta W
$$

$$
\delta Q=d U+\delta W=d U+P d V
$$

$$
c_{v}=\frac{1}{m}\left(\frac{\delta Q}{\delta T}\right)_{v}=\frac{1}{m}\left(\frac{\partial U}{\partial T}\right)_{v}=\left(\frac{\partial u}{\partial T}\right)_{v}
$$

$$
c_{v} d T=d u
$$

## Specific Heats

- Similarly, we can write the following for a constant pressure process:

$$
\delta Q=d U+\delta W=d U+P d V
$$

$$
c_{p}=\frac{1}{m}\left(\frac{\delta Q}{\delta T}\right)_{p}=\frac{1}{m}\left(\frac{\partial H}{\partial T}\right)_{p}=\left(\frac{\partial h}{\partial T}\right)_{p}
$$

$$
c_{p}=\left(\frac{\partial h}{\partial T}\right)_{p}
$$

## Specific Heats



