

1 **Supplementary Material for:**

2

3 **Development and laboratory evaluation of a do-it-yourself (DIY) filtration solution**  
4 **for residential evaporative coolers to reduce indoor wildfire smoke exposure**

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**Figure S1.** Three horizontal-flow (through-the-window/wall) residential ECs acquired for laboratory testing: a-c) Essick RN35W, d-f) Phoenix/Brisa BW4002, and g-i) MasterCool MCP44.

36 **Laboratory Measurements of EC Performance**

37 **Airflow Rates.** An Extech AN200 vane anemometer was used to measure the air velocity leaving  
38 the EC supply at 12 points following a grid pattern at the supply grille. Air velocity measurements  
39 were made with the anemometer approximately 2.5 cm (1 inch) from the face of the supply grille.  
40 The edge points of the grid pattern were at least 4 cm (1.5 inches) away from each edge of the  
41 supply grille. After recording the velocity at the 12 points, an average velocity was calculated,  
42 which was then multiplied by the measured supply grille gross area to estimate the airflow rate.  
43 The uncertainty in airflow rate measurements was estimated using manufacturer-reported  
44 uncertainty for velocity measurements, which is  $\pm$  (3% of reading + 0.2 m/s). We did not propagate  
45 uncertainty for repeated velocity measurements, nor did we estimate the uncertainty in the supply  
46 grille cross sectional area; the former is not customarily done with such repeated measurements  
47 with the same instrument and uncertainty in dimension measurements is challenging to accurately  
48 quantify. The anemometers were purchased new and thus were recently factory calibrated.  
49 Repeatability in airflow rate measurements were investigated by having at least two researchers  
50 periodically repeat velocity traverse measurements at the same test conditions. Three randomly  
51 selected test conditions were initially used to make repeated airflow rate measurements by two  
52 different researchers, which resulted in a mean difference of less than 2% between the  
53 researchers, confirming that airflow rate measurements were repeatable.

54  
55 **Power Draw.** Uncertainty in power draw measurements was taken as that reported by the  
56 instrument manufacturer ( $\pm$ 0.2% of reading). The power draw meters were purchased new and  
57 thus recently factory calibrated. Repeatability for this measure was observed as high by visual  
58 inspection of data at the same conditions.

59  
60 **Pressure Drop.** Uncertainty in pressure drop measurements was taken as that reported by the  
61 instrument manufacturer ( $\pm$ 1% of reading). The DG-700s are approximately 10 years old but were  
62 sent to the manufacturer for calibration in 2022. Repeatability for this measure was noted as  
63 moderate by visual inspection of data at the same conditions, as the tight configuration and  
64 turbulence influenced by the close proximity of the EC fan, pad, and enclosure sometimes  
65 prohibited consistently reliable readings.

66  
67 **Sensible and Latent Cooling Capacity.** The impact of a subset of test conditions and  
68 corresponding airflow rates on sensible and latent cooling capacity of the ECs was evaluated by  
69 measuring the temperature and relative humidity (RH) with Onset HOBO U12 T/RH data loggers

70 logging at 1-minute intervals, located at three points: 1) in front of the EC air intake (i.e.,  
71 upstream), 2) after the cooling pad but before the fan (as a middle point measure), and 3) in the  
72 supply air stream (i.e., downstream, or outlet). Only the inlet and outlet measurements (points 1  
73 and 3) were used to characterize the temperature and humidity differences across the EC during  
74 these tests. Temperature (T) and RH values were used to calculate absolute humidity (W, in units  
75 of kg<sub>w</sub>/kg<sub>da</sub>) for evaluating latent cooling capacity, assuming atmospheric pressure at sea level.  
76 Upstream and downstream values of temperature (T) and humidity ratio (HR, or W) were  
77 averaged over 2 hours of approximately steady-state operational periods at any test condition to  
78 generate a mean and standard deviation (SD) in each value (i.e., upstream and downstream T  
79 and upstream and downstream W). Mean (SD) values in each were used to calculate differences  
80 across the EC, pad, and any filter attachment (i.e., ΔT & ΔW). Values of ΔT and ΔW were also  
81 used to calculate sensible, latent, and total cooling capacity following Equation S1.

82

$$Q_t = Q_s + Q_l = \dot{m}_{da} C_p \Delta T + \dot{m}_{da} h_{fg} \Delta W \quad (S1)$$

83

84 where  $Q_t$  = total cooling capacity (W),  $Q_s$  = sensible cooling capacity (W),  $Q_l$  = latent cooling  
85 capacity (W),  $\dot{m}_{da}$  = mass flow rate of dry air leaving the EC via the supply (kg<sub>da</sub>/s),  $C_p$  = specific  
86 heat capacity of air (J/[kg<sub>da</sub>K]),  $\Delta T$  = temperature difference across the EC, taken as  $T_{supply} -$   
87  $T_{intake}$  (K),  $h_{fg}$  = specific enthalpy of vaporization (kJ/kg<sub>w</sub>), and  $\Delta W$  = humidity ratio difference  
88 across the EC, taken as  $W_{supply} - W_{intake}$  (kg<sub>w</sub>/kg<sub>da</sub>). For the evaporative cooling process,  $Q_t$   
89 should be near zero,  $Q_s$  should be negative, and  $Q_l$  should be positive.

90

91 Uncertainty in temperature and RH was taken as that reported by the instrument manufacturer:  
92 ±0.2°C of reading for temperature and ±2.5-5% of reading for RH (depending on the value of RH  
93 measured). To capture a larger range in uncertainty than experimental uncertainty alone,  
94 propagated uncertainty in ΔT and ΔW was estimated by adding the standard deviations of the  
95 mean upstream and downstream T and W readings in quadrature. Repeatability for this measure  
96 was noted as high by visual inspection of time-series data (i.e., when steady state conditions were  
97 achieved).

98

99 **Tables S1** and **S2** show results for cooling capacity from measurements of temperature and  
100 relative humidity (RH) measured upstream before the EC air intakes and downstream after the  
101 EC supply with the EC operating at approximately steady-state wet conditions under four filter

102 configurations for the Brisa and MasterCool, respectively. The Brisa EC (**Table S1**) was tested  
 103 without a filter (wet pad only), with two deep-bed filters 10-cm (4-inch) filters (Tex-Air MERV 13  
 104 and Rensa CA-13), and with one filtration combination that led to excessive reductions in flow (5-  
 105 cm (2-inch) Tex-Air MERV 13 plus 5-cm (2-inch) Rensa CA-13). The MasterCool EC (**Table S2**)  
 106 was tested without a filter (wet pad only), with two deep-bed 10-cm (4-inch) filters (Tex-Air MERV  
 107 13 and Rensa CA-13), and with a 10-cm (4-inch) Tex-Air MERV 11 as an option that led to a more  
 108 moderate flow reduction.

109  
 110

111 **Table S1.** Mean (SD) temperature (T), relative humidity (RH), and humidity ratio (W) measured before the  
 112 intake and after the supply on the Brisa EC operating at approximately steady-state conditions with a wet  
 113 pad under four filter configurations.

Test Condition	Before Intake				After Supply			Supply - Intake	
	Flow (m <sup>3</sup> /h)	T (°C)	RH (%)	W (g <sub>w</sub> /kg <sub>da</sub> )	T (°C)	RH (%)	HR (g <sub>w</sub> /kg <sub>da</sub> )	T (°C)	W (g <sub>w</sub> /kg <sub>da</sub> )
No Filter	3037 (240)	20.8 (0.2)	65.1% (1.8%)	10.0 (0.3)	18.4 (0.3)	86.9% (1.0%)	11.5 (0.4)	-2.4 (0.4)	1.5 (0.5)
Tex-Air 4" MERV 13	2812 (233)	21.6 (0.1)	66.4% (1.2%)	10.8 (0.2)	19.1 (0.5)	88.5% (0.2%)	12.2 (0.2)	-2.5 (0.5)	1.5 (0.3)
Rensa 4" CA MERV 13	2656 (228)	22.0 (0.1)	67.1% (0.1%)	11.0 (0.1)	19.5 (0.1)	88.9% (0.4%)	12.6 (0.1)	-2.5 (0.1)	1.6 (0.2)
Tex-Air 2" + Rensa 2" M13 Combo	2573 (226)	21.6 (0.1)	66.1% (0.2%)	10.4 (0.2)	19.0 (0.1)	87.8% (0.5%)	12.0 (0.2)	-2.6 (0.1)	1.6 (0.3)

114

115 Results from the Brisa show that regardless of filter attachment and associated airflow rate, the  
 116 difference in temperature and humidity ratio between the intake and supply air were similar, with  
 117 a temperature drop of approximately 2.5°C and an increase in humidity ratio (W) of approximately  
 118 1.5-1.6 g<sub>w</sub>/kg<sub>da</sub> in the lab environment regardless of test condition. This suggests that delivered  
 119 cooling capacity is affected only by airflow and not by synergistic or antagonistic effects due to  
 120 changes in ΔT or ΔW.

121

122 **Table S2.** Mean (SD) temperature (T), relative humidity (RH), and humidity ratio (W) measured before the  
 123 intake and after the supply on the MasterCool EC operating at approximately steady-state conditions with  
 124 a wet pad under four filter configurations.

Test Condition	Before Intake				After Supply			Supply - Intake	
	Flow (m <sup>3</sup> /h)	T (°C)	RH (%)	W (g <sub>w</sub> /kg <sub>da</sub> )	T (°C)	RH (%)	W (g <sub>w</sub> /kg <sub>da</sub> )	T (°C)	W (g <sub>w</sub> /kg <sub>da</sub> )
No Filter	2900 (258)	25.0 (0.8)	38.3% (4.7%)	7.5 (0.4)	20.4 (0.8)	62.6% (2.6%)	9.3 (0.2)	-4.6 (1.6)	1.9 (0.5)
Tex-Air 4" MERV 11	1862 (219)	23.5 (1.5)	43.5% (5.5%)	7.7 (0.4)	18.3 (0.5)	71.6% (2.1%)	9.3 (0.1)	-5.2 (1.6)	1.6 (0.4)
Tex-Air 4" MERV 13	1862 (219)	27.3 (0.3)	33.0% (0.7%)	7.4 (0.2)	20.1 (0.2)	67.2% (0.4%)	9.8 (0.1)	-7.2 (0.4)	2.4 (0.3)
Rensa 4" CA MERV 13	1458 (204)	26.9 (0.6)	33.0% (0.8%)	7.3 (0.2)	20.0 (0.5)	67.4% (0.9%)	9.8 (0.2)	-6.9 (0.8)	2.6 (0.2)

125 Results for the MasterCool were not as clear and were likely affected by higher variability in  
 126 environmental conditions upstream of the air intakes but did not suggest systematic impacts of  
 127 airflow rates on  $\Delta T$  or  $\Delta W$ . For example, while the Tex-Air 10 cm (4-inch) MERV 11 and MERV  
 128 13 filters were measured to have approximately the same airflow rate,  $\Delta T$  was 2°C higher and  
 129  $\Delta W$  was nearly 1 g<sub>w</sub>/kg<sub>da</sub> higher with the MERV 13, not because of airflow but likely because of a  
 130 higher entering temperature when the MERV 13 was tested (the air entering the ECs in these  
 131 tests was surrounding lab air and thus temperature was not precisely controlled). If any  
 132 relationship can be ascertained, it is that the measurements conducted with filtration attachments  
 133 that decreased flow rates demonstrated slightly larger  $\Delta T$  and  $\Delta W$  than no filter conditions.  
 134

135  
 136 **Particle Removal Efficiency.** Two sets of paired OPCs were used for efficiency testing in the  
 137 laboratory including one pair during 2022 (prior to summer 2022 pilot testing in the field) and  
 138 another pair after pilot testing and before full deployment in summer 2023 (two different OPC  
 139 pairs were used because one OPC was damaged while in the field in 2022). Prior to each round  
 140 of laboratory testing, the two paired OPCs were calibrated against each other using co-location  
 141 tests in which both devices were placed in the same location for a period of time (ranging from  
 142 about 30 to 90 minutes, logging at 1-minute intervals) to measure the same ambient indoor  
 143 aerosol sample, and a linear regression between the two devices was used to generate co-  
 144 location calibration factors for each size bin (**Table S3**). Only co-location factors with R<sup>2</sup> above  
 145 0.85 were used; factors with R<sup>2</sup> below 0.85, which were present for the two largest size bins in

146 the second round of testing due to very low number concentrations, were excluded and only raw  
147 concentration measurements were used for those size bins.

148  
149 **Table S3.** Co-location factors for paired MetOne OPCs used in laboratory filtration efficiency  
150 measurements.

Bin size ( $\mu\text{m}$ )	Prior to Summer 2022		After Summer 2022	
	Slope	R <sup>2</sup>	Slope	R <sup>2</sup>
0.3-0.5	0.875	0.94	0.803	0.99
0.5-1	1.022	0.98	0.856	0.99
1-2.5	0.838	0.97	0.921	0.97
2.5-5	0.887	0.95	0.949	0.91
5-10	1.228	0.96	0.739	0.65
10+	1.233	0.86	0.382	0.21

151  
152 **VOC Removal Efficiency.** Sample air was introduced to the PTR-ToF-MS drift tube at 250  
153 mL/min via a 9 m long section of 0.64 cm o.d. PFA tubing heated to 60 °C. The PTR-ToF-MS  
154 scanned across 17–490 amu for compounds with proton affinity higher than that of H<sub>2</sub>O using  
155 H<sub>3</sub>O<sup>+</sup> as the primary reagent ion. The operating conditions were as follows: T<sub>drift</sub> = 60 °C, P<sub>drift</sub>  
156 = 2.20 mbar, and U<sub>drift</sub> = 600 V, which resulted in electric field strength to number density ratio  
157 E/N = 135 Td (Townsend, 1 Td = 10<sup>-17</sup> V.cm<sup>2</sup>). Signal intensities of NO<sup>+</sup> (m/z = 29.9970), O<sub>2</sub><sup>+</sup>  
158 (m/z = 31.9892), and the water cluster (H<sub>2</sub>O)H<sub>3</sub>O<sup>+</sup> (m/z = 37.0289) were respectively about 0.2%,  
159 2%, and 2.5% of the H<sub>3</sub>18O<sup>+</sup> (m/z = 21.0221) one. The mass axis was calibrated using a  
160 hydronium isotope, H<sub>3</sub>18O<sup>+</sup> (m/z = 21.0221), NO<sup>+</sup> (m/z = 29.9970), and a C<sub>6</sub>H<sub>4</sub>I<sub>2</sub> fragment (m/z  
161 = 203.944), which is an internal standard continuously injected into the drift tube via a heated  
162 permeation device (PerMaScal, Ionicon Analytik GmbH, Innsbruck, Austria). Mass spectra were  
163 stored in ten-second intervals. Mass spectra were analyzed using PTRViewer 4.0, with VOC  
164 peaks elevated due to wildfire smoke identified and corrected for isotopic interferences and  
165 quantified using calibration factors determined from a calibration standard that contained BTEX  
166 compounds (Apel-Reimer, USA).

167



168  
169 **Figure S2.** Chamber test setup for measuring VOC removal efficiency of a new 10 cm (4 inch) depth  
170 carbon-impregnated MERV 13 filter at Portland State University.

171  
172 Chamber background concentrations for benzene and toluene were identified visually either  
173 before or after decay periods after a short period of approximately steady-state operation. Linear  
174 regressions on the natural log transformed concentration data versus time were used to estimate  
175 first order loss rate constants during each of the four test conditions, using Equation S2.

$$-\ln\left(\frac{C_{i,in}(t) - C_{i,in,bg}}{C_{i,in}(0) - C_{i,in,bg}}\right) = L_i t \quad (S2)$$

177  
178 where  $C_{i,in}(t)$  = the concentration of constituent  $i$  at time  $t$  (ppb),  $C_{i,in}(0)$  = the concentration of  
179 constituent  $i$  at time  $0$  (ppb),  $C_{i,in,bg}$  = the steady-state concentration of constituent  $i$  at a given  
180 test condition (ppb),  $L_i$  = first order loss rate constant for constituent  $i$  (1/min), and  $t$  = time since  
181 the beginning of constituent decay (min). The CADR for constituent  $i$  at each of the three tested  
182 face velocities was then estimated using Equation S3.

$$CADR_i = V(L_{i,test} - L_{i,no\ filter}) \quad (S3)$$

184  
185 where  $L_{i,test}$  and  $L_{i,no\ filter}$  = the estimated first order loss rate constants for constituent  $i$  in the  
186 chamber during a given test condition and without the fan/filter combination operating,  
187 respectively,  $V$  = the interior volume of the test chamber ( $17.8\text{ m}^3$ ), and  $CADR_i$  = the CADR for  
188 constituent  $i$  at the test condition ( $\text{m}^3/\text{min}$ ). Finally, the single-pass VOC removal efficiency for  
189 constituent  $i$  was estimated using Equation S4.

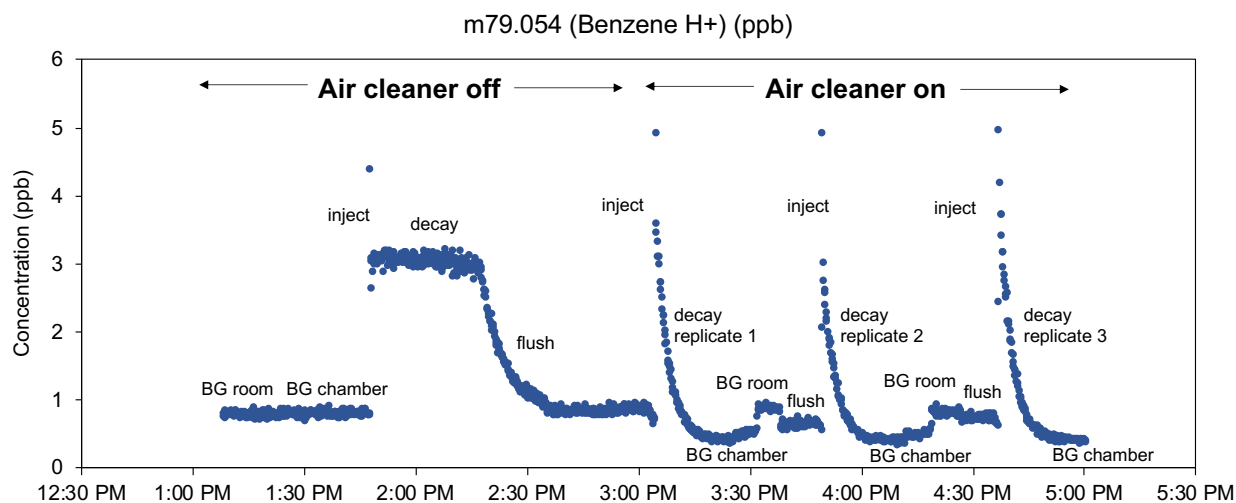


190

$$\eta_i = \frac{CADR_i}{Q_{filter}} \times 100\% \quad (S4)$$

191  
192 where  $\eta_i$  = is the estimated single-pass removal efficiency of the filter for constituent  $i$  at a given  
193 test condition (-) and  $Q_{filter}$  = the measured flow rate through the filter at a given test condition  
194 ( $m^3/min$ ).

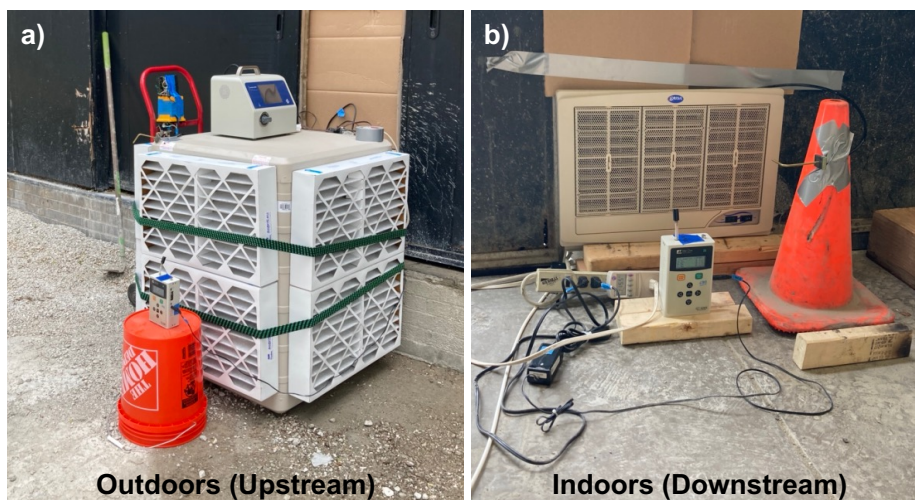
195  
196 **Figure S3** shows an example of time-resolved benzene concentrations measured by the PTR-  
197 ToF-MS during chamber testing of a 61x76-cm [24x30-inch] 10-cm [4-inch] depth Rensa CA-13  
198 carbon-impregnated MERV 13 filter and fan combination at Portland State University. The first  
199 half of the figure shows benzene elevation (by burning pine needles) followed by natural decay in  
200 the enclosed chamber without the fan/filter combination operating, followed by a flush with  
201 ambient room air surrounding the chamber. The second half of the figure shows three replicate  
202 elevation and decay periods using the same source but with the fan/filter combination operating.  
203 The PTR-ToF-MS device switches between chamber and room conditions at the end of each test  
204 and the chamber is flushed with room air in between tests. Chamber background (BG)  
205 concentrations are selected by visual observation, including BG chamber measurements just  
206 before pollutant elevation during the period with the fan/filter switched off ('air cleaner off') and  
207 BG chamber measurements at the last few minutes of each decay period with the fan/filter  
208 operating ('air cleaner on').



209  
210 **Figure S3.** Example of benzene concentrations measured by PTR-ToF-MS during chamber testing of  
211 Rensa CA-13 carbon-impregnated MERV 13 filter and fan combination at Portland State University. BG  
212 room = background in room outside of chamber, BG chamber = background.

213 **Wildfire Event in Chicago, IL.** On two days with heavy wildfire smoke in Chicago, one of the test  
214 ECs (Brisa BW4002) was rapidly deployed just outside a set of exterior doors of their laboratory  
215 building on campus and fabricated a sheath to mimic a through-the-wall installation of an EC  
216 (**Figure S4**).

217



218

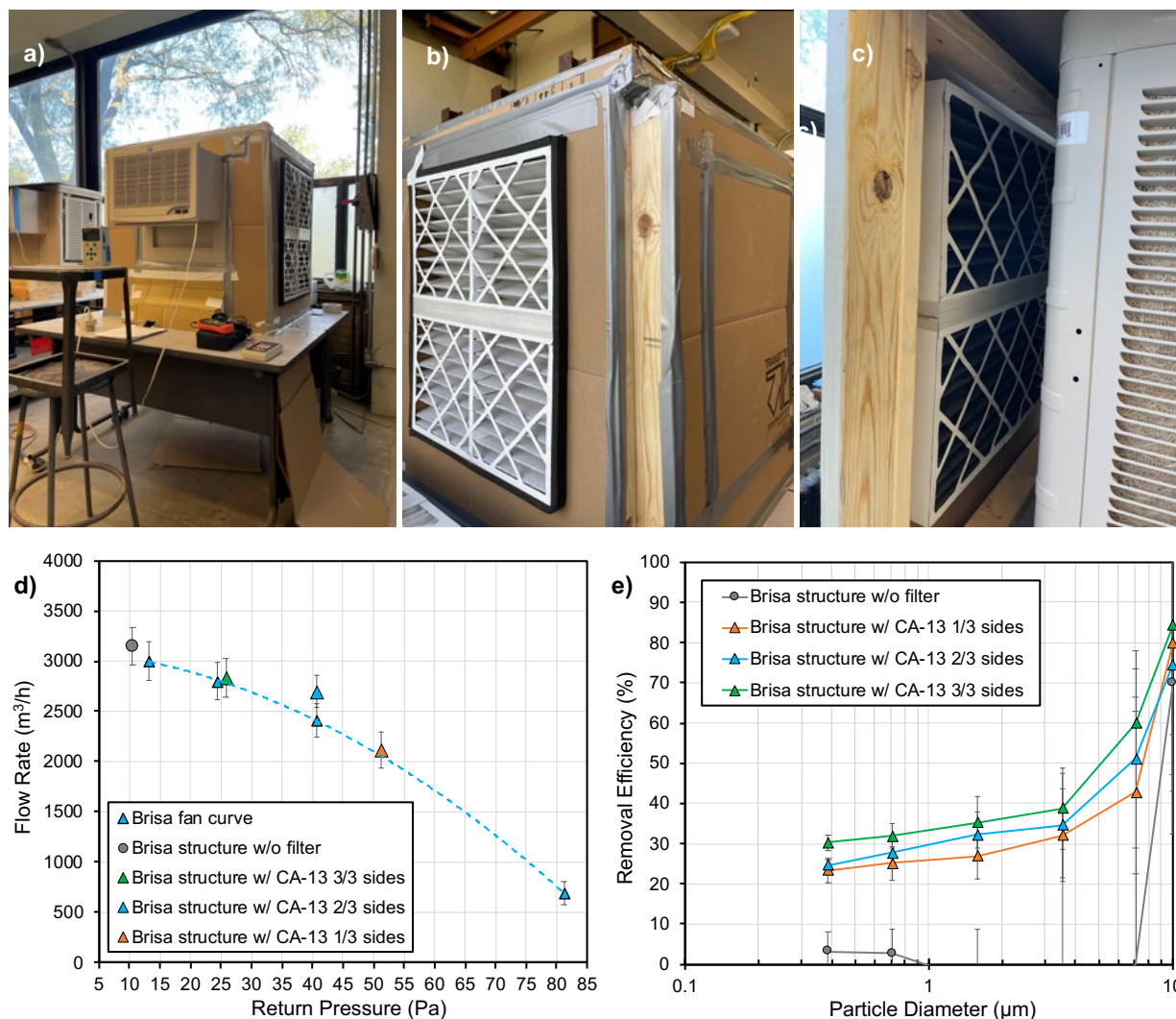
219 **Figure S4.** Brisa BW4002 EC and particle monitors (SMPS and two OPCs) deployed outside IIT's  
220 laboratory to conduct measurements during the heavy smoke conditions caused by long-range transport  
221 from Canadian wildfires to Chicago on June 26-27, 2023: (a) outdoors (upstream) and (b) indoors  
222 (downstream).

223

#### 224 **Testing a plenum structure to house filters**

225 **Figure S5** shows results from testing a custom surrounding structure that could act as a plenum  
226 and filter housing and allow for filter(s) to be offset from the ECs, potentially reducing moisture  
227 issues and leading to longer filter lifespans. A surrounding structure was constructed out of  
228 cardboard on just the Brisa unit, allowing for installation of filters on any of the three intake sides.  
229 This allowed for evaluating not only the impact of the filters installed in the surrounding structure  
230 on performance metrics, but also for evaluating different combinations of filters with varying levels  
231 of blockages to better understand the minimum number of filters through which ECs could draw  
232 airflow through and still achieve flow performance targets. Therefore, this solution was tested  
233 under four conditions, including: (1) three structure openings completely open (mimicking 0%  
234 blockage but with the structure in place), (2) filter installed on one intake opening with the other  
235 two intakes blocked, (3) filters installed on two intake openings with the other blocked, and (4)  
236 filters installed on all 3 intake sides of the structure. These configurations were also chosen for  
237 their potential to reduce filter costs, i.e., if only one or two filters could be installed in a larger

238 structure but still maintain flow and efficiency goals, then the upfront filter cost could be reduced.  
239 Only the 10-cm (4-inch) Rensa CA-13 filter was tested for these purposes. The structure is shown  
240 visually in **Figure S5a-c**. **Figure S5d** shows results from airflow rate testing at these four  
241 conditions overlaid on the original Brisa fan curve that was regenerated by progressive blocking  
242 and **Figure S5e** shows size-resolved removal efficiency measured across the EC under these  
243 test conditions.  
244



245  
246 **Figure S5.** Test results from a custom surrounding structure that could act as a plenum and filter housing  
247 and allow for filter(s) to be offset from the ECs: a-c) photos, d) airflow versus pressure drop, e) size-  
248 resolved particle removal efficiency.

249